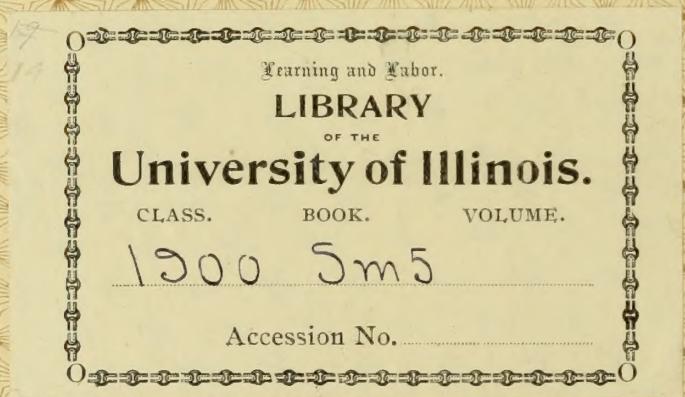


SMITH

Use of Compressed Air
for Pumping Water

Mechanical Engineering
B. S.

1900





THE USE OF COMPRESSED AIR
FOR PUMPING WATER

... BY ...

GEORGE RUSSELL SMITH

THESIS

FOR THE DEGREE OF BACHELOR OF SCIENCE
IN MECHANICAL ENGINEERING

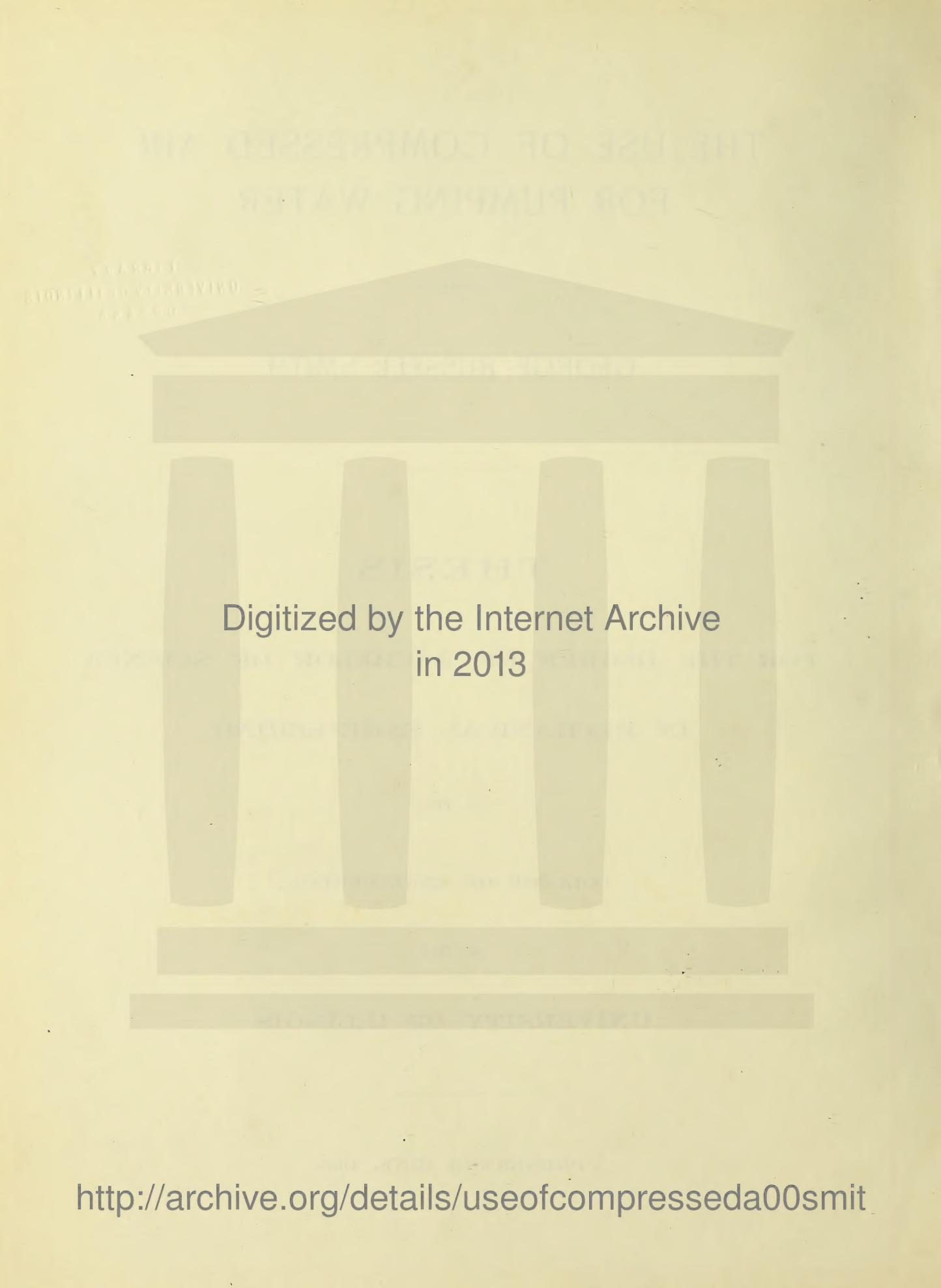
IN THE

COLLEGE OF ENGINEERING

OF THE

UNIVERSITY OF ILLINOIS

PRESENTED JUNE, 1900



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May 31, 1900. 190

THIS IS TO CERTIFY THAT THE THESIS PREPARED UNDER MY SUPERVISION BY

George Russell Smith

ENTITLED The Use of Compressed Air for Pumping Water

IS APPROVED BY ME AS FULFILLING THIS PART OF THE REQUIREMENTS FOR THE DEGREE

OF Bachelor of Science in Mechanical Engineering.

L. P. Breckinridge

HEAD OF DEPARTMENT OF Mechanical Engineering.

Table of Contents.

	Page.
HISTORICAL	1-21
Frizell patent,--	2
Siemens patent,--	3
Pohle and Hill patents,--	4
Plate 1, Pohle and Hill pump,--	6
Plate 2, " " " " ,--	7
Plate 3, Pohle pump,--	8
Plate 4, Three methods of well piping,--	9
Kennedy patent,--	10
Plate 5, Kennedy nozzle,--	11
Saunders patent,--	12
Plate 6, Saunders well piping,--	13
Haas patent,--	14
Bickel patent,--	14
Titus patent,--	14
Harris patent,--	15
Plate 7, Harris pump,--	17
Merrill patent,--	18
Plate 8, Merrill pumps,--	19
Elliot patent,--	20
Plate 9, Elliot pump,--	21
TESTS OF COMPRESSING AIR BY FALLING WATER AND RAISING WATER BY COMPRESSED AIR,--	22-44
AIR COMPRESSING BY FALLING WATER, J. P. Frizell,--	22-28
Plate 10, Frizell apparatus for air compressing,--	23
Table 1, Results of experiments in air compressing,--	26
Table 2, Comparison of observed and computed losses of head,--	27



16

Table of Contents.

AIR LIFT IN CALIFORNIA,-----	1
Composition of air at 70° F. using smooth tubulated pipes,-----	13
Table 5, The effect of changing the volume of air,-----	20
Table 6, Tests of air lifts at industrial plants,-----	21
AIR LIFT IN CALIFORNIA,-----	36-44
Table 11, Positive air lift pump,-----	37
Table 7, Receiver pressures for different compression ratios,-----	38
Table 8, Total air lift delivered per stroke,-----	39
Table 12, Apparatus used to measure air lift,-----	40
Table 9, Air delivered per second required from the pump,-----	41
Table 10, Results of tests of the air lift, in California,-----	42
Table 11,-----	43
Table 12, Method of using more than one lift in deep wells,-----	44
TESTS OF THE AIR LIFT AT PUMPING STATION,-----	45-50
Table 13, Pumping stations,-----	46
Table 14, Air lift delivered,-----	47
Table 15, Pumping stations,-----	48
Table 16, Air lift delivered,-----	49
Table 17, Pumping stations,-----	50
TESTS OF THE AIR LIFT OF THE CHAMPAIGN AND URBANA WATER COMPANY, AT URBANA,-----	51-59
Table 18, Location of pumping stations,-----	52
Table 19, Preliminary results,-----	53
Table 20, Air lift delivered,-----	54
Table 21, Pumping stations,-----	55
Table 22, Air lift delivered,-----	56
Table 23, Pumping stations,-----	57
Table 24, Air lift delivered,-----	58
Table 25, Pumping stations,-----	59

The principle of raising a column of water by the direct pressure of compressed air has been known since the sixteenth century, but the practical application of it has been made within quite recent years. In the use of air for water elevating two general methods have been employed. In one, water and air are admitted alternately, to a chamber, which is provided with suitable valves for admitting water and discharging air alternately, and for admitting air for compressing water, and discharging water for supplying the air, under pressure, to the lower end of a valve-riser and thus elevating the water.

In Austria, in 1886, the "Berg und Hüttenmännische Zeitung", December 4th, 1886 stated that the air system of water elevating was first used in the sixteenth century. In the "Zeitschrift des Vereins Deutscher Ingenieure" of November 16th, 1885, Berlock states that this system of water elevating was described in 1797 by Dr. Emanuel Jässcher, a mining engineer, of Freiberg, as an hydrostatic drainage apparatus, by means of which water can be raised several ells without any buckets or pumps". The experiments of Jässcher were made by submerging a rising pipe for part of its length, in the water, in a tank and then blowing air through a small tube into the submerged opening of the first pipe. The bubbles of air became mixed with the water, in the rising main and diminished its specific gravity so that the mixture of water and air was driven high above the water level in the tank by the hydrostatic pressure, and, under certain conditions was made to flow out from the riser. In 1846 an American, Mr. Crawford made use of this same principle in raising

from drilled wells in Pennsylvania.

A United States patent granted for an air pump was issued on the 10th of October, 1880 and issued to Mr. Joseph F. Frizell, Member of the American Society of Civil Engineers, for a "Method of Raising Water". Mr. Frizell has previously worked out a method of air compressing, by using a vertical column of water. A patent was granted to him for this on June 29th, 1872. The method employed for the air compressing will be more fully described below. The patent for a method of raising water by means of compressing air naturally followed that of using water for compressing air.

The claim allowed on the Frizell patent of 1880 was as follows: "In the art of elevating water the method of causing a column of air to ascend in a conductor by the weight of the external water, which consists in introducing a tube of the desired length and a required depth into the water to be elevated, and then introducing compressed air in the form of minute bubbles into the water at the lower end of said tube, thereby raising the water, so that a continuous stream is caused to flow upward to the point of elevation substantially as described".

Substantially the same invention as that of Mr. Frizell was made, and a patent issued to Prof. W. H. Harris, of Little Rock, Arkansas, of the Missouri School of Mines. While sinking the piers for the foundation of a bridge over the Arkansas river, near Pine Bluff, Arkansas, Prof. Harris used air of compressed air for pumping out the water and sand. A 3 inch pipe 20 feet long was set vertically, with the upper end about 4 feet above the surface of the water and the lower end resting on the sand bottom at a depth

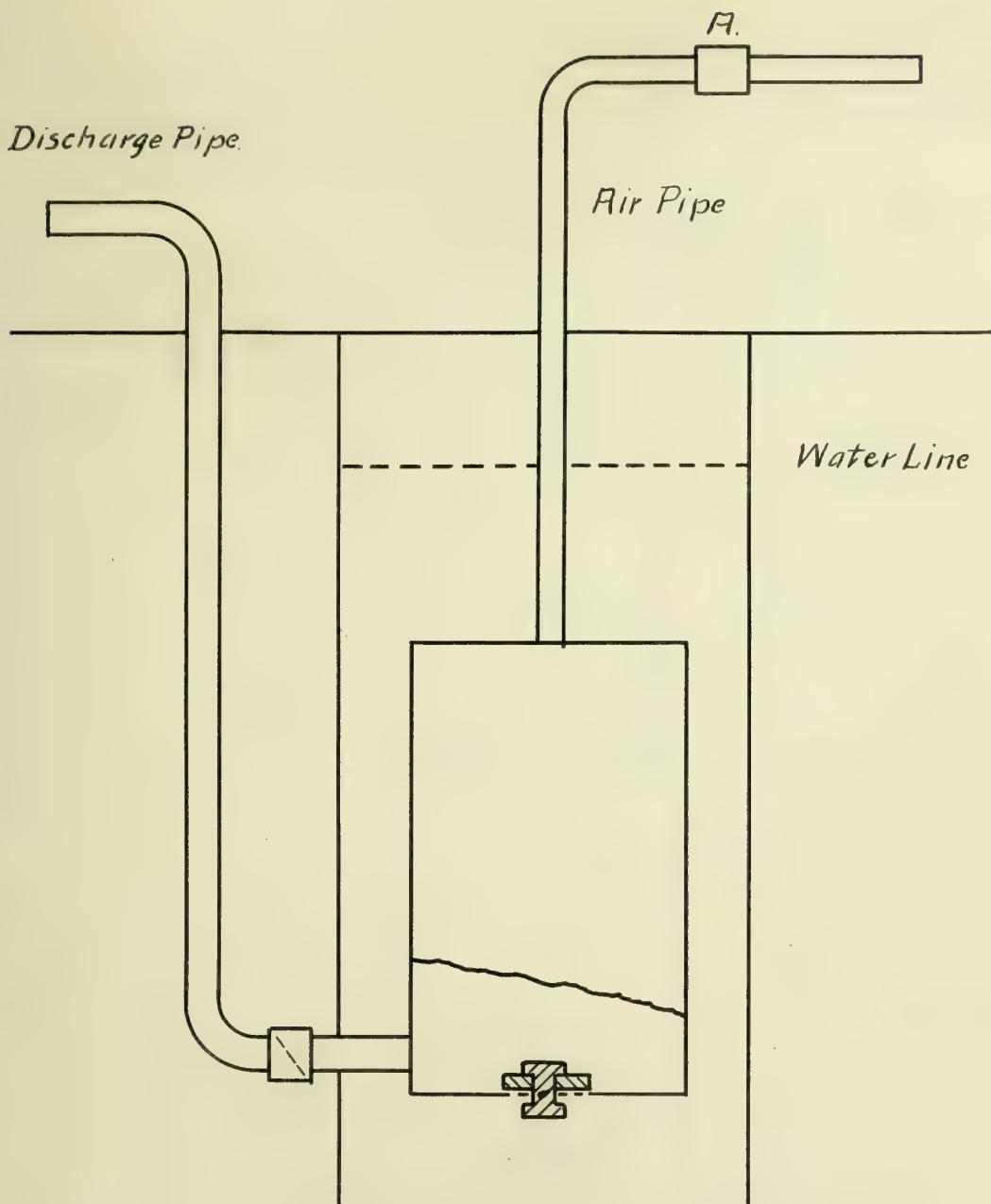
feet. About 4 inches above the lower end of the large pipe a hole was cut and a 1 inch pipe was forced into the large pipe at right angles to it. Into this small pipe air was forced by means of the ordinary pump and hose connections used for pumping the air to the divers' helmet. An abundant discharge was obtained, from the top of the large pipe, which was estimated by the divers to contain about equal parts of sand and water. A patent was applied for by Mr. Harris and was first refused by the Patent Office on the ground that Mr. Frizell's application had been first presented, but the final rejection was based upon the fact that the patent, already referred to and also the patent of Captain C. C. Frizell, No. 2,000,000, was prior art.

Another patent was taken out by Mr. Harris, No. 2,000,415, the last two being for hydraulic excavators. A similar invention was made by Dr. Siemens, - see abstract in Proceedings of the Institution of Civil Engineers, volume 81, page 400, 1885 taken from "Dinglers Polytechnische Journal" volume 111, page 284. In a coal shaft being sunk near Berlin, 30 meters below the bearing sand had to be gone through. The shaft became flooded. It was attempted at first to relieve the pressure on the shaft by making numerous Abyssinian wells in the surrounding alluvium, but these owing to their small size did not permit of sufficient water being taken out. Dr. Siemens, of imitating the action of gas springs, geyser, and petroleum wells, in nature. His plan was to convey compressed air to the bottom of the suction pipe and there allow the air to escape through the mass of water, where by its expansive action a sufficient force would be exerted, until an equilibrium was obtained. The pressure was obtained.

the glassy scinian tube wall, that had been for some time in use, the tube being 20 millimeters, depth 30 meters and it had a suction lift of 3 meters long. The tube was lengthened 9 meters and a lead pipe 20 millimeters in diameter, terminating in a copper wind-hole with numerous small holes was put down to the bottom. This was connected with an air compressor, which was turned by reversing the action of a portable steam engine. Regarding the action of the lift Dr. Siemens says: "As soon as air is sent in the air vessel rose to three atmospheres, a current was established, the air sucked from the bottom of the suction pipe into the water in the well tube and rose slowly in numerous bubbles. As each bubble exerted a pressure on the water representing it equivalent to that of the water it displaced, the water was raised to the surface of the air vessel. Air was sent into the pipe, overflowing it if the water was not too high. The velocity of the water which is constant so long as the air current is kept up, depends upon the quantity of air supplied per unit of time, and the frictional resistance in the tube and the air vessel."

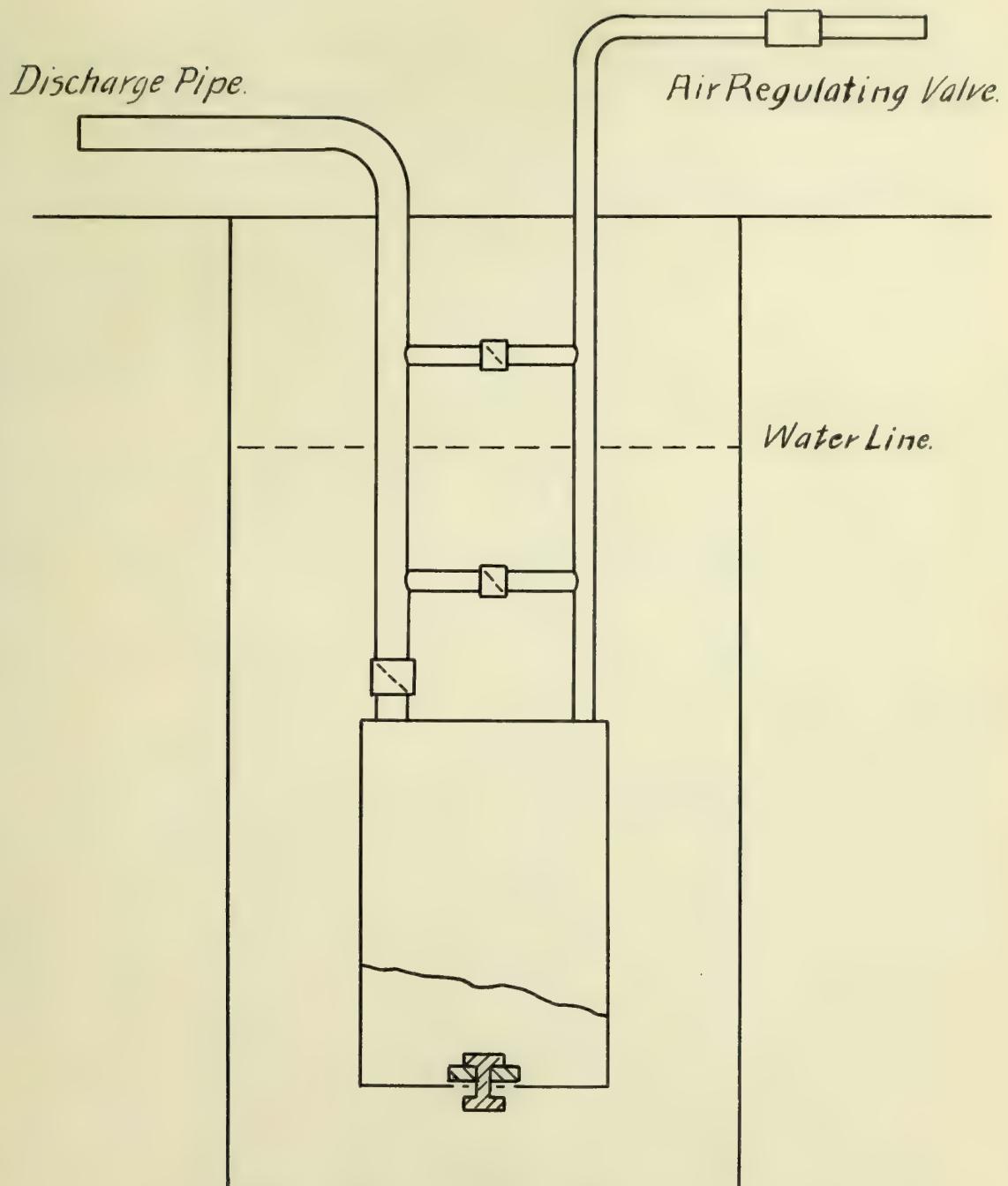
This method was first used in France. Gauvry was granted a patent for the use of nitric acid by means of it, the apparatus being known as "emulsion pump."

The inventor who has also used the air lift pump into practical use is Dr. Julius G. Pohl. While manager of some California mines Dr. Pohl discovered that in the operation of an old pneumatic pump, an advantage was gained by introducing compressed air into the discharge pipe. A patent number 354,895 was granted March 23rd, 1886 to Messrs. Pohl and Hill for a form



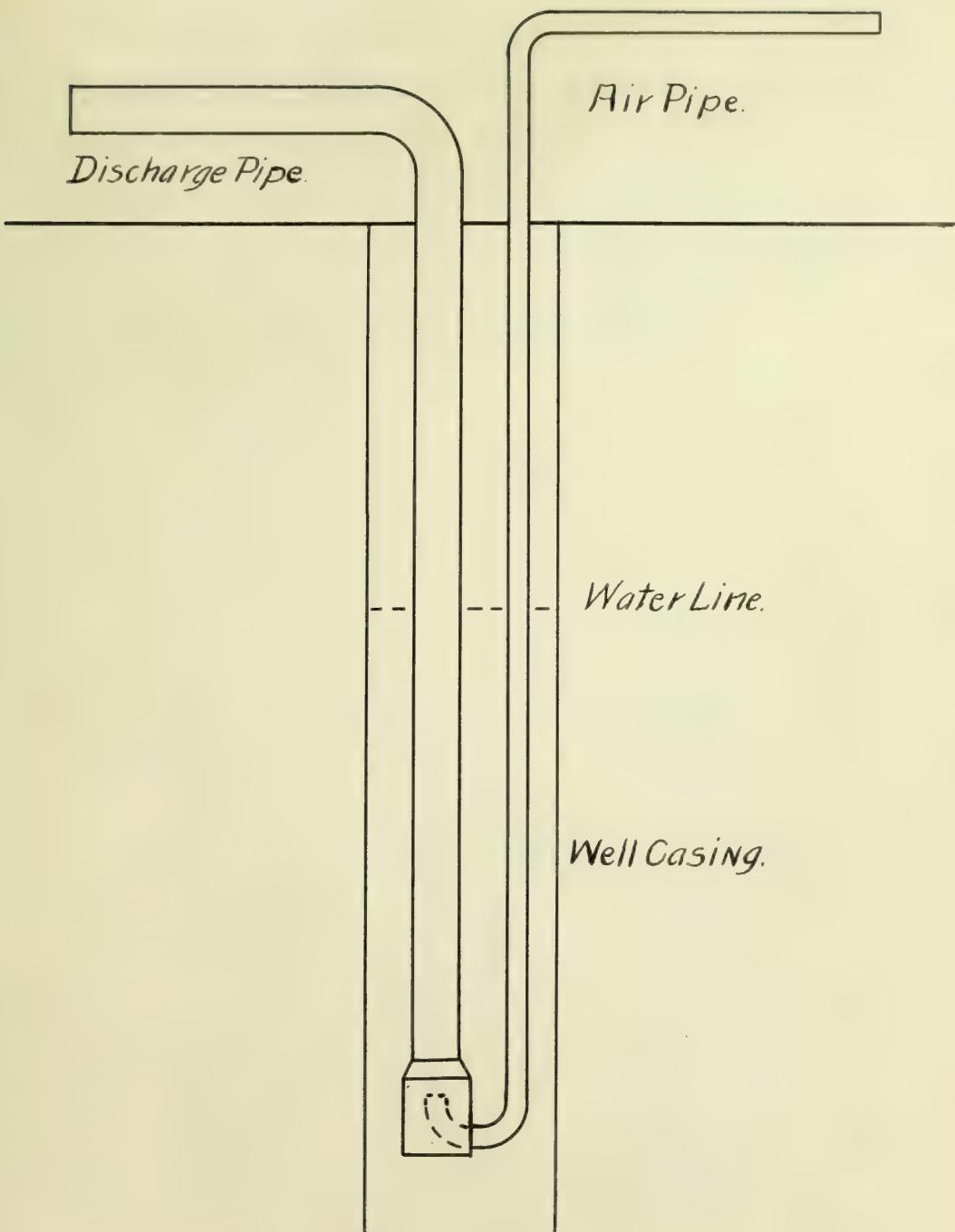
Pohle Patent Number 338295.

Plate 1.



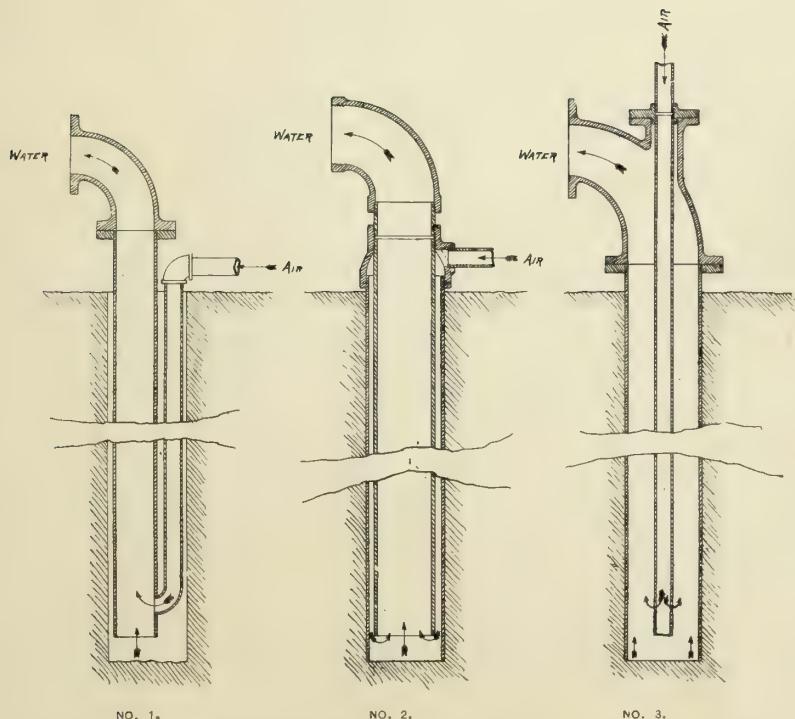
Pohle and Hill Patent. Number 347,196.

Plate 2.



Pohlé Patent, Number 487,639.

Plate 3.



THREE METHODS OF WELL PIPING.

Plate 4.

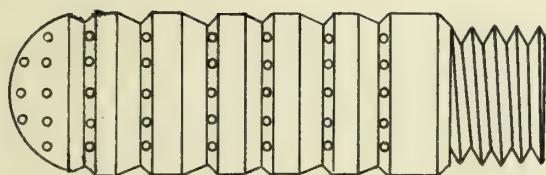
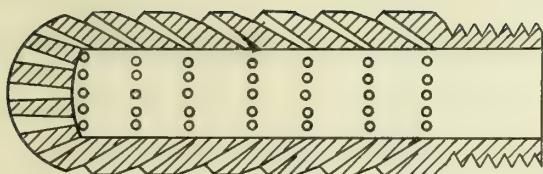


Figure 4.

Kennedy Nozzle.

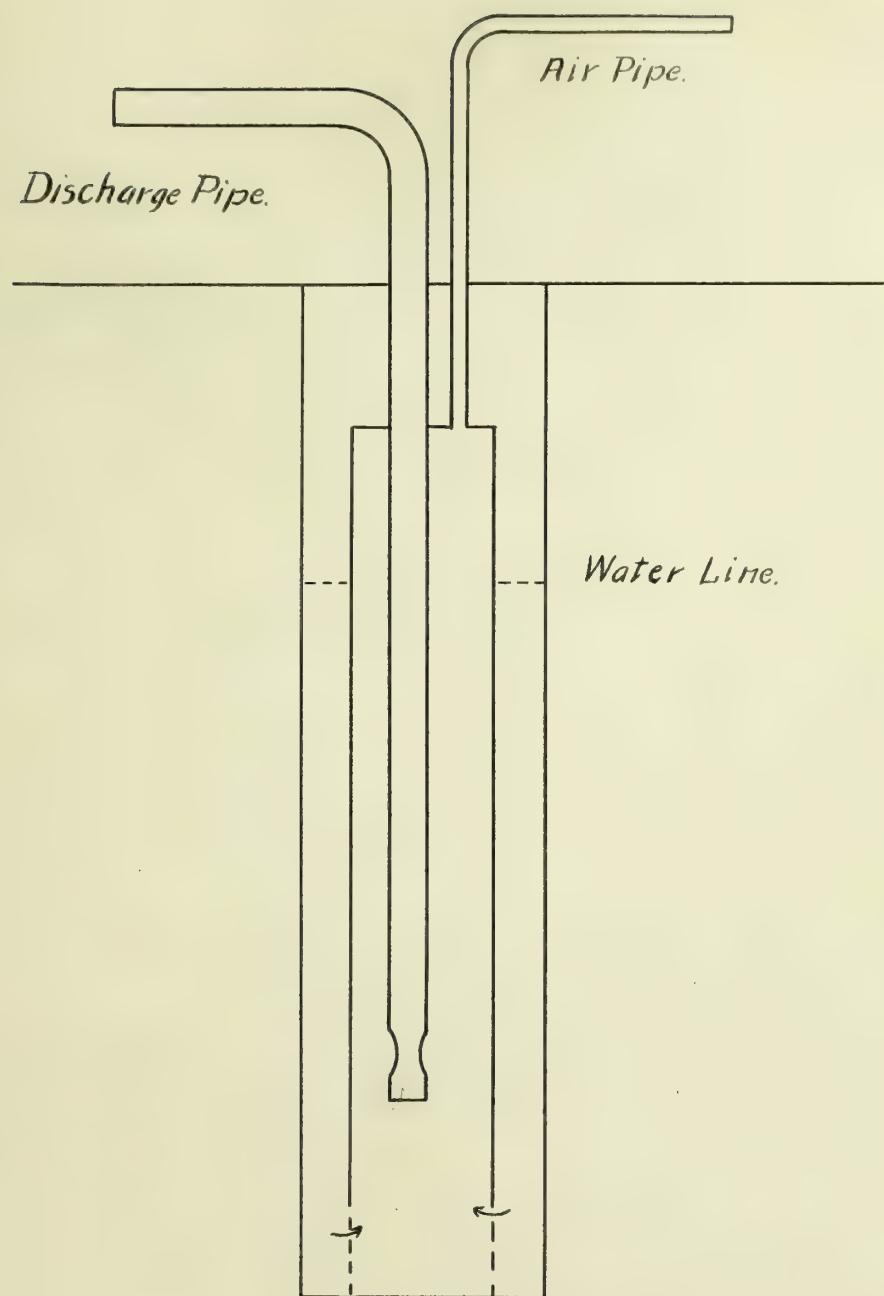
Patent Number 568,445.

Plate 5.

W. J. KENNEDY, of South Plainfield, N.J., was granted on
July 10, 1900, patent No. 790,721, for an "Air Lift Pump". The
claims, taken from the patent record, which are given, are
as follows: I claim—

1.— The herein described method of pumping which consists
in pumping, through an open lower end of a tubeless de-
livery pipe surrounded by an open bottom chamber continuously
filled with gas under pressure, of charges of the liquid and of
water pressure and the air therein.

2.— In an air lift pump the combination of a stationary
delivery pipe formed with a contracted portion nearer its lower
end, a pressure chamber surrounding said pipe, said chamber
being partly open at its lower end to receive the water, and valve-
less connections between the pressure chamber and an independent
source of compressed air at one end, and with the water at the
bottom, whereby the level of the liquid will be determined in the
chamber and the pressure of the air from the tank will always exceed
the liquid pressure within, causing the liquid to be maintained
at the lower end of the delivery pipe, so that water may
therefore be taken.



Saunders Patent Number 597,023.

Plate 6.

of several different points throughout its course,

it may be injected into the suction tube at different times, also a series of cut-offs or valves adapted to open or close the air line at one or more of the different points and a means for operating the cut-offs or valves.

Reference is made to G. Morris, who has been mentioned for his work

in connection with the air lift, in a United States patent, number

107, on April 13th, 1897 for a pump. Claim number four of

is as follows: "A pump, consisting of

two vessels each having at its bottom a pipe connector

admitting and discharging water, and each having at its top a

connection for admitting and discharging air; a switch connecting the air-vessel or said vessel with the other pipes leading

to inlet and discharge, respectively, of an air-compressor, said

switch being adapted to reverse the connections of said air-

with said pipes leading to the inlet and discharge of an air-

compressor, and an valve for automatically operating said switch

between the medium of atmospheric pressure in conjunction with a

partial vacuum created in the intake pipe of the compressor, said

valve comprising a cylinder, piston and piston-rod, a valve arm

connected to admit free air to propel the piston and to allow the op-

erating air to escape into the intake pipe of the compressor, said

valve being operated by a rod connected at one end to the said

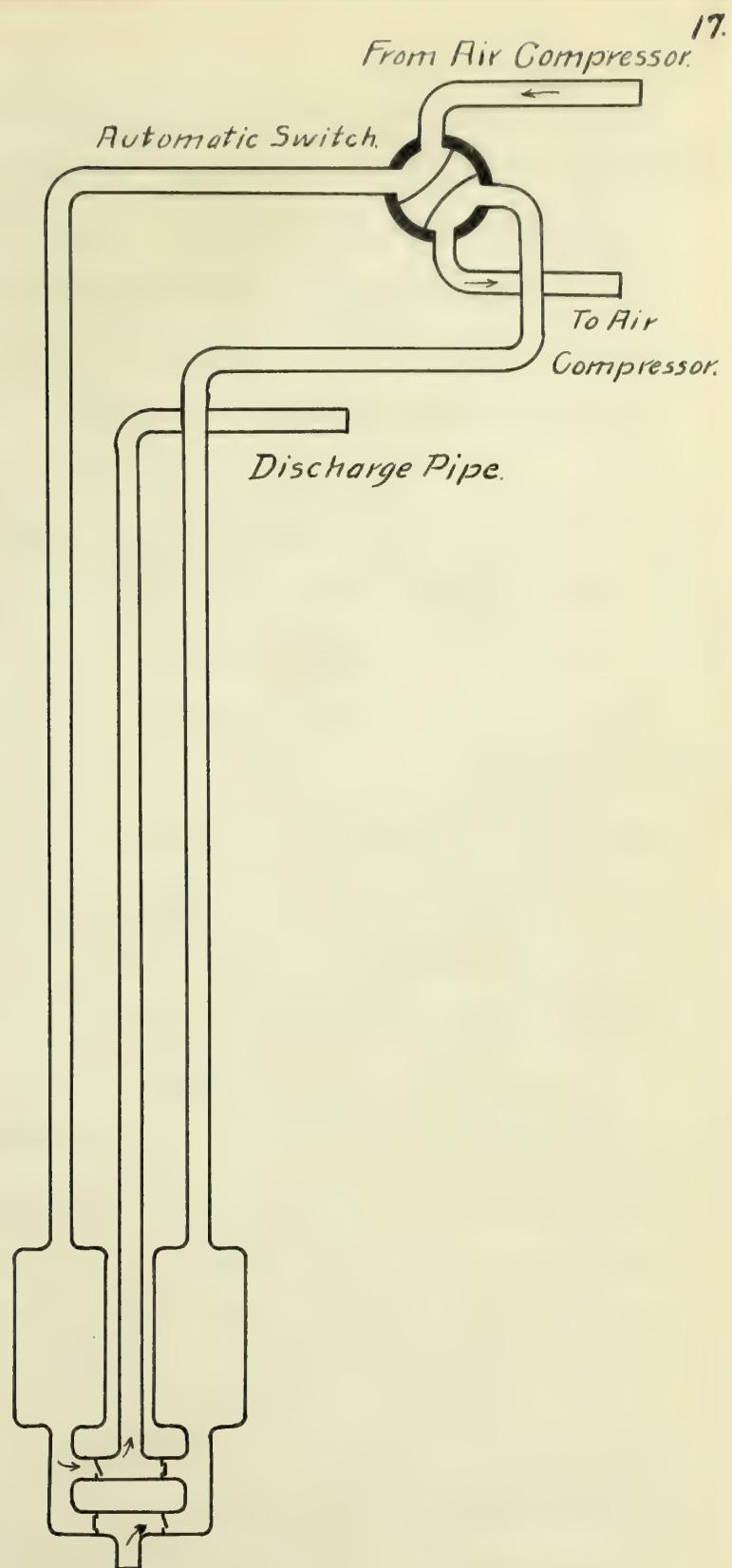
valve arm and at the other end to a weight, the weight being used to operate the valve; and an adjustable weight mounted between the vertical guides above said piston-rod and connected thereto by a

link which in its extreme positions is inclined so that said weight

will hold said valve arm in the position of the valve being closed.

essentially as described".

While it does not give a drawing of the actual working pump, serves to show the relative position of the different parts. Professor Baum's pump is the most simple direct-air-pressure pump, because the liquid first flows in closed vessels. It is then drawn out and forced by the action of compressed-air. The pump has no floats or air-valves of the engine room and no means of selection to ensure that the air from the tanks returns to the compressor, and the air entering the pump is intended to run the pump. The air enters from an automatic switch which turns the air from the capital tank to the other, and at the same time turns the exhaust air back to the capital tank. The switch can be operated by means of the pressure of air, in the inlet pipe to the compressor, provided, when the air in either tank is drawn above the normal level, or by a mechanical device, operated by a pressure gauge or the inlet to the compressor, or a float in one of the tanks or a mechanism through the switch after a fixed number of strokes of the piston. The designer computed the loss of power in the working of the pump to be 15.4 per cent. This includes the loss due to friction in both air and water pipes, and to the drop in pressure after the switching, but not including the loss in the compressor. The basis, on which this estimate was made, was on a pump to raise 1000 gallons per minute through a vertical height of 100 feet, the length of both air pipes and of the water pipe being 1200 feet.



Harris Displacement Pump.

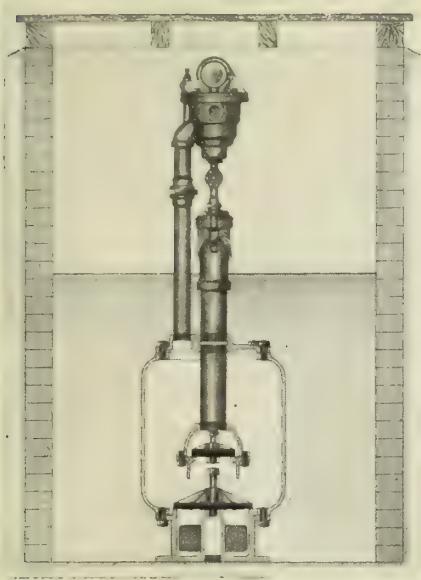


Figure 1.

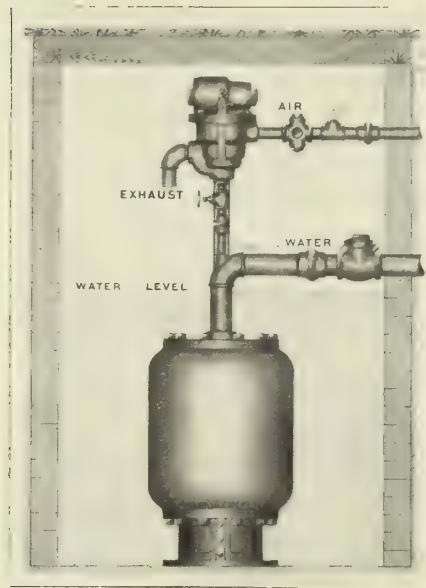
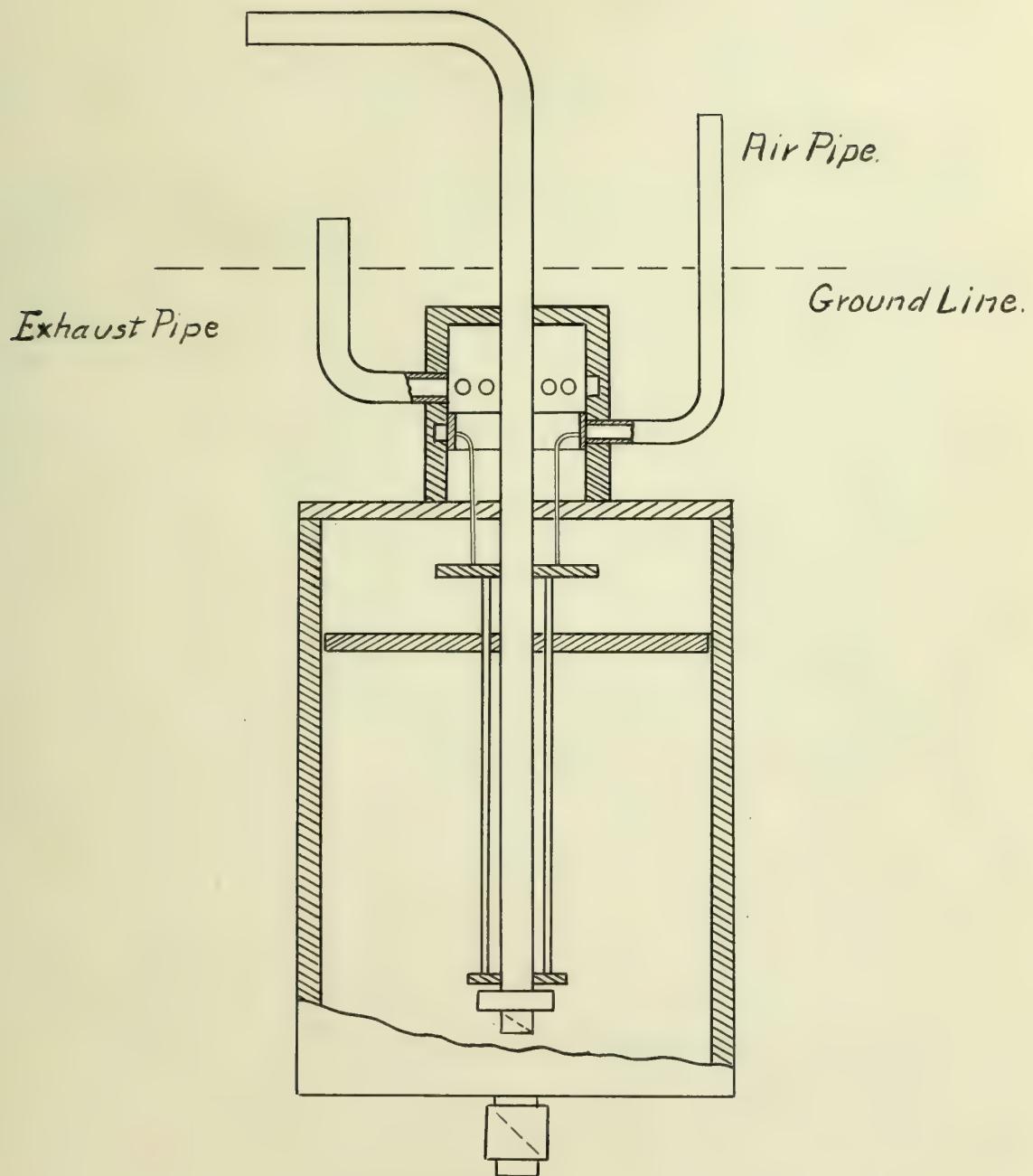


Figure 2.

Merrill Single Acting Displacement
Pump.

Plate 8.



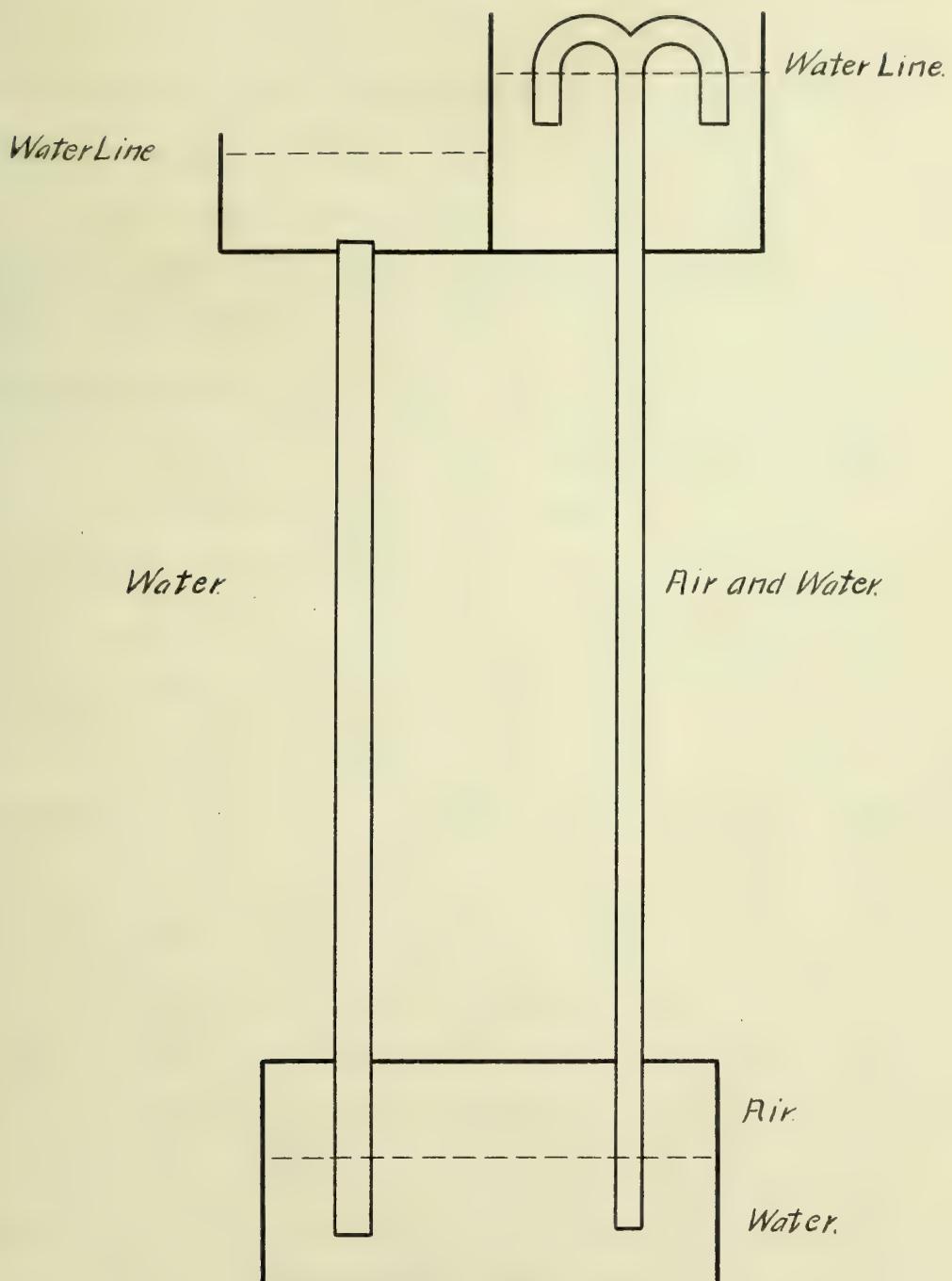
Elliot Displacement Pump.

Journal of the American Water and Raisin Water by
Government Agents.

Journal of the American Water and Raisin Water.

At the time of the great Boston fire, Mr. Prizell first attempted to fly, but the apparatus he then used was first attempted by Mr. Joseph P. Prizell about 1870. He succeeded this time in getting off, but the ascent was caused to pass down a vertical passage. At the foot of this fall the direction was changed to horizontal, then to the vertical again and升到了 such a height as to give the required expansion. Placed between the vertical sections and on the upper side of the horizontal part of the apparatus, in which the air was collected, as it escaped from the vertical, Mr. Prizell's flight was, at the commencement, very rather slow. For vertical passages between 30 and 35 feet in elevation he was slow. The difference in level between the upper openings of the vertical sections was about 16 inches and the height of the sections 3 feet and 3 feet. The efficiency of the apparatus was considered to be between 5 and 10 per cent. A larger apparatus was constructed by Mr. Prizell and after being exhibited in Boston, was sent to the hydraulic laboratory of the Massachusetts Institute of Technology, Boston, to cause the examination of the apparatus.

After the examination of the apparatus, the company obtained permission, from the government officials to use the apparatus during the Boston fair, and as a



Frizell Method of Air Compressing by Means of
a Vertical Column of Water.

gives the observed and computed losses. The agreement is not perfect in the observations in the experiments with velocities exceeding 7 feet per second, since in these cases large quantities of air were carried past the cylinder involving corrections not taken account of in the computation. In the experiments giving the best results, the agreement is quite satisfactory.

Table II.

Losses of Head as Observed and Computed.

Observed Head.	Computed Head.
2.24	2.22
3.12	3.12
3.52	3.51
4.82	4.77
4.70	4.82
4.99	4.95
4.91	4.93
4.87	4.77
4.79	4.67
4.70	4.77
5.03	4.92

The same of computation was then applied to a series of parallel shafts 10 feet in diameter, taking the mean

times that of the water. Assume shaft in the water 100 feet, head 15 feet. Velocity in descending shaft 150 feet per second. The head should be less than 15 feet in design taken, to avoid loss of head, such as air rounded entrance to the descending shaft.

Friction head is directly proportional to the square of the velocity, directly as the distance traversed by the water, and inversely as the mean radius of the channel. The other losses proportional to the square of the velocity.

This gives in the proposed system the following losses:

$$\text{Head loss} \left\{ \frac{16}{(4.40)} \right\} x (x^2 + 3) = 1.870 \text{ feet.}$$
$$\text{Head loss} \left\{ \frac{16}{(4.40)} \right\} \frac{R}{(1.62)} = 0.741 \text{ "}$$

$$\text{Total head loss} = 1.870 + 0.741 = 2.611 \text{ feet.}$$
$$\text{Total head loss, } \frac{2.611}{150} = 0.0174 \text{ feet.}$$

$$\text{Efficiency} = \frac{1 - 0.0174}{1} = 78 \%$$

Similarly for a head, corresponding to a pressure of 100 pounds per square inch, efficiency would be 81 %.

Some experiments and computations tend to show that when a pump is run on a large scale an efficient compressor would be found.

Tests of the Air Lift in Germany.

On the 20th of October 1881, and 18th, 1882, comparative tests of an air lift by comparison with a vertical pump were given in the "Zeitschrift" of the German Society of Engineers.

Two sets of tests of the air lift were made. The first were laboratory tests, the object being to find the efficiency of the lift under given conditions; the other tests were made under ordinary working conditions in actualized plants.

Laboratory comparative tests were made using smooth and ribbed pipes. The computations were clear around the pipe, so that its cross section was everywhere circular, although of variable diameter. The claim was made for this pipe that its larger form enabled a greater amount of water to be raised, than was possible, with a smooth pipe, because the computations would allow the drops of water from slipping back during the general upward movement of the air and water. The well was 10.1 inches in diameter and 98.4 feet deep. In this were placed the air and water pipes and for determining the level of the water during the test. Above the well was built a tank of 100 feet 6 inches, which was placed a tank. From this tank a connection was made to the air lift. The air pipe was suspended in a tackle, so that the amount of submergence and free lift could be altered. This arrangement made it possible to measure the discharge, the free lift and the submergence. The length of the air lift from the well to the lift was about 150 feet. As there were no valves in it a ratchet was attached to the line just

is 200 ft. entered the well in order to enable the air pressure to be exerted.

Exploratory tests first undertaken were carried out (1) with a smooth 4-inch r.p.s. pipe 119.75 feet long and corrugations of 0.11 and 3.01 inches in minimum and maximum diameter, (2) with a smooth discharge pipe 2.73 inches in diameter, and (3) with a lift having a smooth discharge pipe of the same length and 2.07 inches diameter.

Three sets of tests were made with the three lifts which differed in the ratio of the height of the lift to the depth of submergence. Three separate experiments were made in each set, which differed only in the amount of air furnished, the ratio of lift to submergence being kept constant. The amount of air furnished was computed from the number of strokes of the air piston, and was taken from the air cylinder, which gave the volumetric efficiency. The results of the tests are given in Table 4. As explained the tests showed that the corrugated pipe was a hindrance rather than an advantage. It is evident that the corrugated pipe offers increased resistance to the rising mixture of water and air than the smooth pipe, because with the latter the greatest efficiency between the indicated work in the compressor and the work done in the water raised was 45 per cent, while the corrugated pipe under similar conditions gave but 28.7 per cent. The nozzles used in the two cases were different. With the smooth discharge pipe the nozzle was of bronze, the form being such that the air was discharged around the entire circumference of the pipe, while in the other case the air was introduced into the discharge pipe by a simple U bend at the bottom of the air pipe, with the air end in the center of the riser. In order to determine

In the case of this different construction, in the case of smooth bore pipe, the brass nozzle was put on the corrugated pipe. It was found that with large air supplies and correspondingly large discharge of water there was no difference, but that with the normal air supply the common nozzle furnished 25 per cent. more water.

After the completion of these experiments a lift was constructed with a discharge pipe 3.1 inches in diameter, a submergence of 1.2 feet and a free lift of 24.6 feet. The brass nozzle was used in these experiments. Table 5 gives the results obtained with this lift.

Table 5.

The Effect of Changing the Volume of Air.

Volume of Air, Gallons per minute.	Free Lift, Feet.	Submergence, Feet.	Cubic Feet per minute.	Volume of Air per Gallon of Water.
24	29.06	24.61	7.6	0.26
25	79.25	"	18.6	0.24
26	96.43	"	28.2	0.29
27	101.17	"	33.7	0.31
28	112.54	"	44.3	0.39
29	116.24	"	50.6	0.44
30	116.24	"	55.8	0.48
31	117.01	"	57.7	0.50
32	105.67	"	106.0	1.00

Following the laboratory experiments, tests were made at four industrial establishments. The results of these experiments are given in Table 6.

Table 6.

Tests of Air Lifts at Industrial Plants in Germany.

Test	Locality	Barometric Pressure, feet.	Velocity of Air, feet per minute.	Capacity, cubic feet per minute.	Pressure, pounds per square inch.	Efficiency
32	Glogau	94.88	42.91	6.30	2.99	556.37
33	"	92.82	44.91	6.30	2.99	741.79
34	"	94.68	42.91	6.30	2.99	722.72
35	"	94.88	42.91	6.30	2.99	798.35
36	Zwickau	63.32	44.91	7.56	4.84	1075.20
37	Bochum	201.84	202.10	2.01	0.92	43.95
38	Wittenbergen	493.55	229.66	2.44	1.34	65.14
						45.3
						176.4
						19.1

(The following two columns should be on right of above table)

Efficiency %
Velocity of Water at Nozzle
Feet per Second.

82.3	5.7
84.3	7.2
80.1	3.0
14.9	8.9
21.6	4.6
20.0	4.3

Table 6 gives the following data: The velocity of air in the pipe 1 : 1, in the others 2 : 2. The efficiency is the ratio between

work done in the air cylinder of the compressor and in raise-

The efficiency of the Glogau compressor ranged from

45.3% in test 33 to 83.6% in test 36. (Probably mechanical effi-

Comparison of tests 11 and 57 in which the lifts and air capacities were approximately alike and only the capacities were different, being 39.7 and 1073.2 gallons a minute respectively, shows that the amount of air needed to raise each gallon of water and the efficiency were in close conformity. It may be therefore assumed that with all capacities and all lifts between 15 and 50 feet, the volume of free air needed will be two or three times the volume of water raised.

It is also shown by tests 33 and 34. The difference in efficiency may be attributed to the different relative submergence. As the lifts of Zwicker and Glegau are nearly the same the depths of submergence differ by about 33 feet, and because the greater depth calls for higher air pressure and hence more work for the compressor without the corresponding increase in the distance of the lift, it is at once apparent that this is the cause of the smaller efficiency at Glegau. From these tests it is evident that the ratio of submergence to lift is soon to be between 1 : 1 and 1 : 2. With increasing lifts the air consumption rises and the efficiency falls.

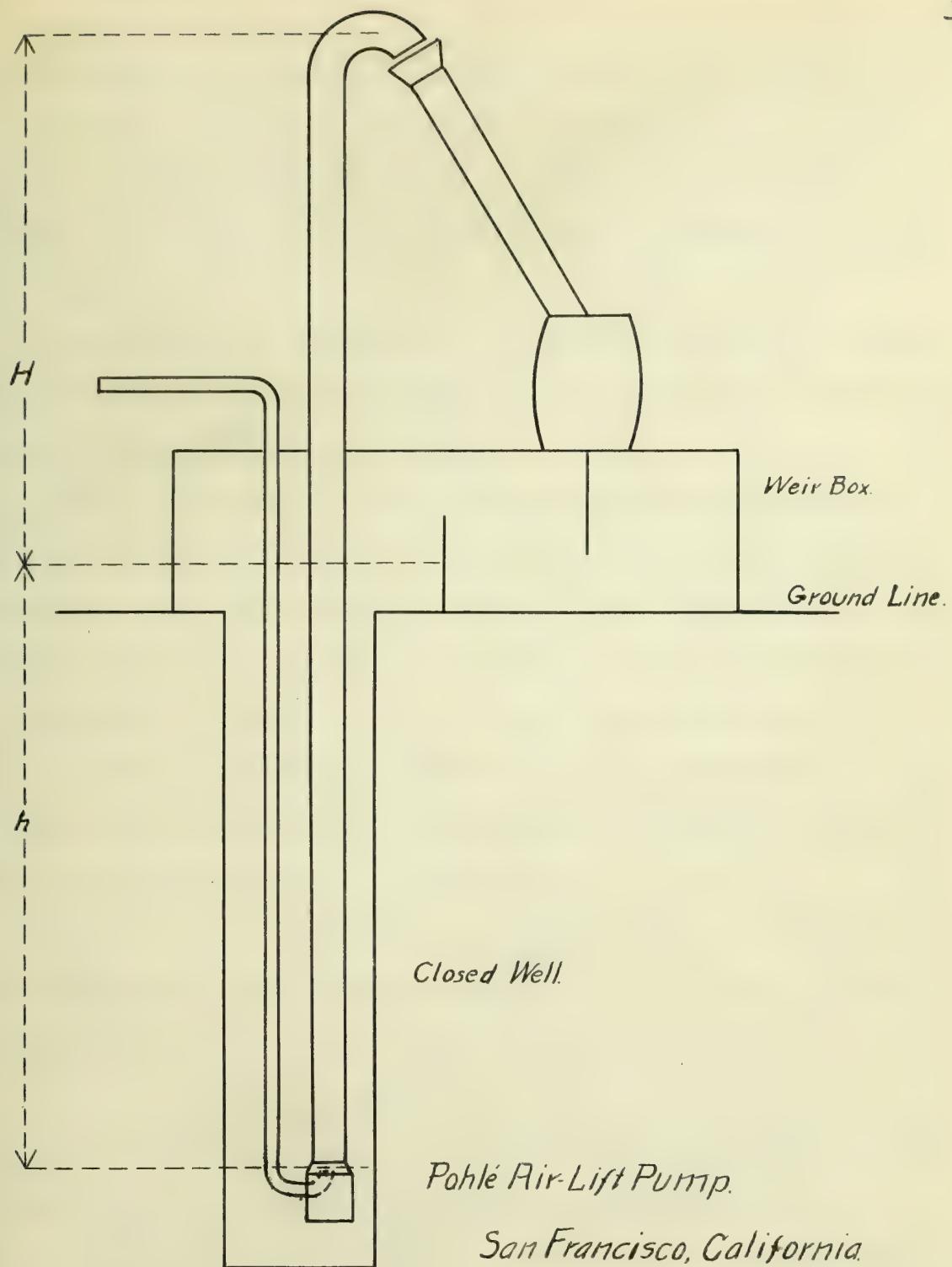
In plotted curves of the laboratory tests it was shown, that the range of the apparatus at first increased to a maximum in consequence of the air supply and then fell off when still more air was furnished. It was also shown by a curve that the maximum discharge was reached when the quantity supplied per lift was small compared with its total capacity. With a discharge of 30 or more than 100 gallons a minute the air supply was not strongly related to the quantity of water raised.

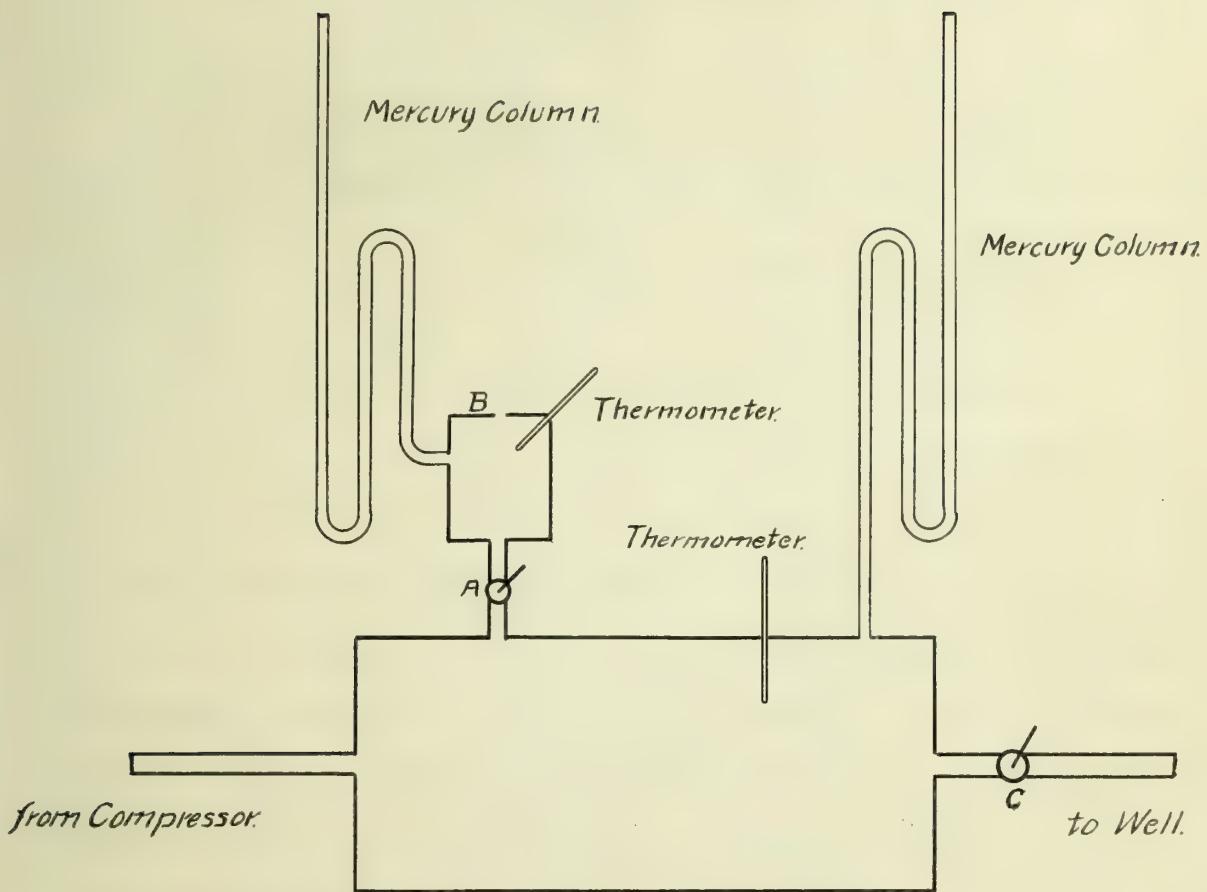
The best economy or the highest ratio between the work done in

THE AIR LIFT AND ITS EFFICIENCY.

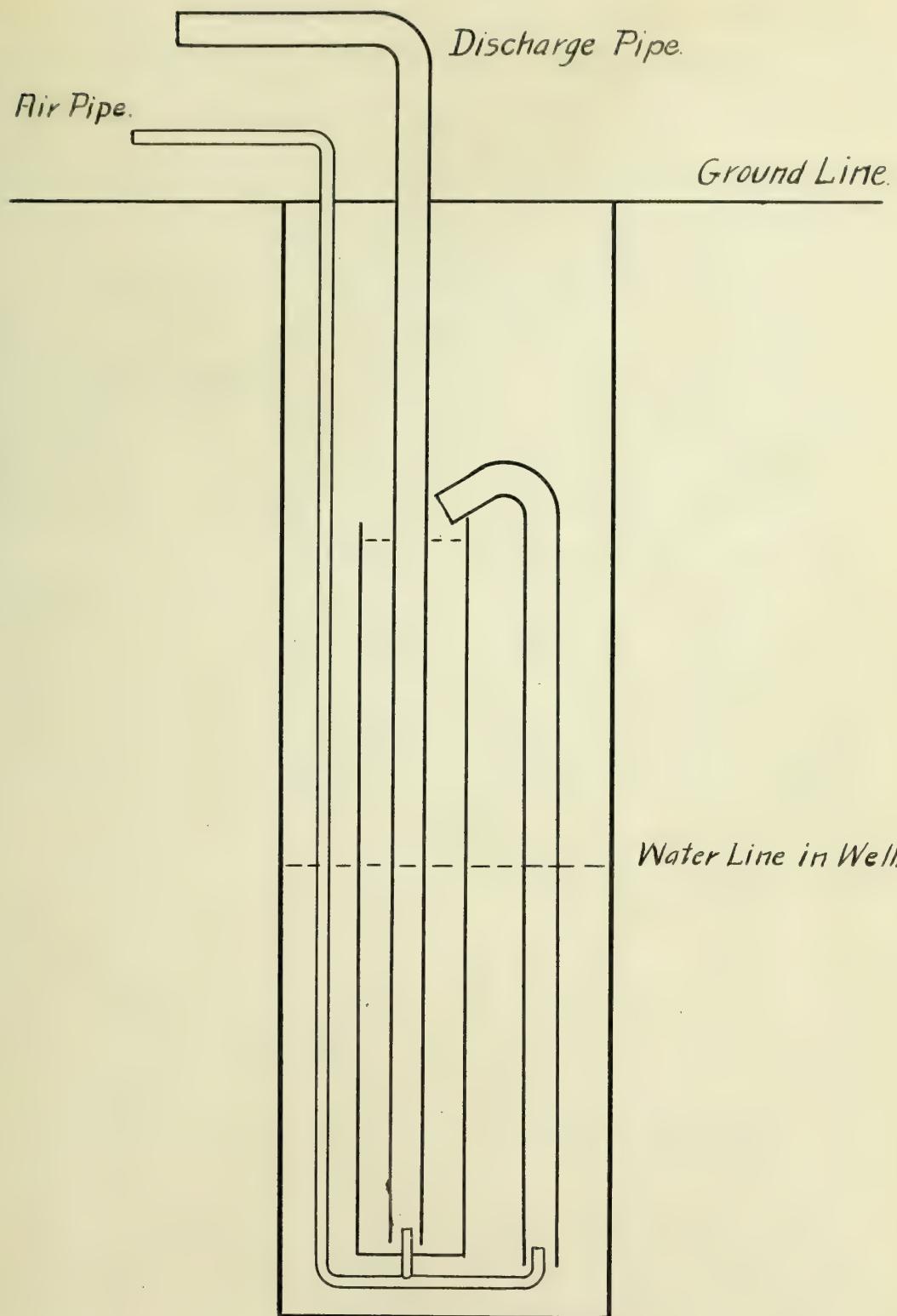
The tank is the most extensive ever made in this country. Dr. Andrew's exhibit of the air lift was made at the Alameda California Fair, October 18, 1898, 1000 feet. Randall of San Francisco made a careful investigation of the theory and practical use of the pump. His reports being favorable an experimental tank was set up in San Francisco. The tanks were made by Prof. Randall, who was aided by Messrs. Ross E. Brown and Harry C. Penn. In 1899 Mr. Brown read a paper before "The Technical Society of the Pacific Coast" giving the results of the tests. A little later Prof. Randall read a paper before the same society giving a more detailed discussion of the lift. On account of its length this paper was not published in the society's proceedings.

The top part of the apparatus used in the test is shown in Figure 11. The diameter of the discharge pipe was 3 inches; of the air pipe 0.9 inches; and of the air nozzle $5/8$ inches. The air pipe had four bends, and a length of 35 feet plus the depth of immersion. The water was passed from a steel pipe well (25 feet deep and 10 inches in diameter) discharged into a tank and deposited over a quayental weir back to the well. The air pipe was arranged that it could be raised and lowered, thus giving different ratios of lift to submersion. The record was not paid the best proportion, and it is probable that the efficiency could have been increased by a few slight alterations. The air pipe should not have been reduced at the discharge end as the nozzle necessitated a greater pressure in the receiver than would otherwise be required.





Apparatus for Measuring the Quantity of Air Delivered
by the Compressor.



Method of Using More Than One Lift in Deep Wells.

that a relation exists between the efficiencies in the use of compressed air to pump water, and in the reverse case, that of pumping air by water. In both cases it is shown that the efficiency is greatest when the work is done on a large scale. It was indicated by Mr. Brown after their tests in California that when different compressors were used in parallel, the efficiencies were those of the experimental lifts, an efficiency of over 100% could be obtained. A conclusion, quite similar, was reached by Mr. Howell from computations obtained after his tests on air compressing had been made at the Anthony Falls, Minneapolis.

The Brown experiments and the Howell experiments show that the efficiency is greatest when the ratio of lift to depth of compression is about 1 : 1. They also show that the air pressure should be equal to the pressure due to the height lifted, and that the volume of air delivered determines the efficiency.

the air lift of the air pump and pump water company,
Champaign, Illinois,
January 10th, 1901.

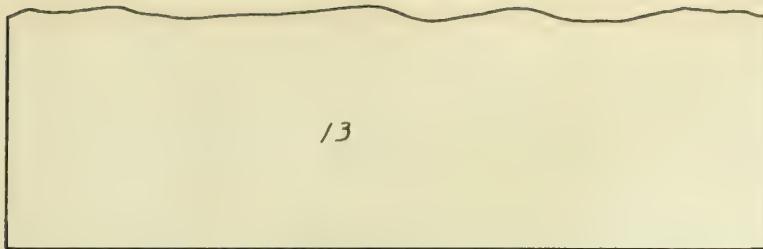
The subject of the air lift was first taken up at my suggestion, some laboratory tests concerning different kinds of
piping, and different methods of piping, were made, when having
done this, I then made a trial air lift, to determine what
was the place and suitable apparatus for such work. A test of
the air lift at the Champaign & Urbana Water Pumping station
was arranged for and made. The plant is located in the north
part of town on the north side of the Big Four Railway.
The water is raised from wells about 165 feet deep, into
a reservoir of 250,000 gallons capacity and from there pumped into
the air lift. The average daily requirement at present is about
1,000,000 gallons of water per twenty four hours.

For two years since the water supply was not equal to the demand, no additional wells were drilled, and four of them connected with an air compressor which was then installed. Within the last two years it has been found necessary to again increase the capacity of the plant. This time geared, electrically driven deep well pumps are to be substituted for the air lift wells, and also a part of the steam deep well pumps that are now in use.

At the time the test was made there were in operation two pressure tanks, one a "Worthington" & the other a "Gordian and Maxwell"; two 12" double acting deep well pump, two "Boat" deep well pumps and three air wells. Two "cock" pumps had been disconnected the week before.

Fig. 14 shows the location of the air compressor, receiver, air tank and reservoir. The manner of piping at the wells is shown

3○



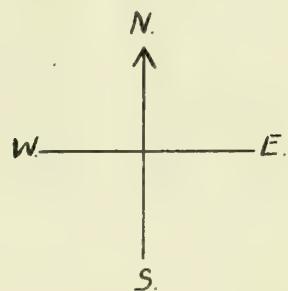
○4

2○

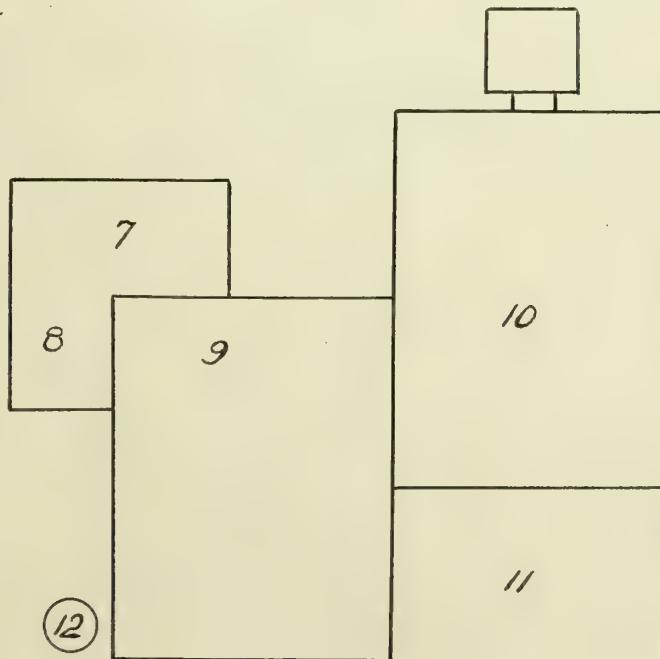
5○

○1

- 1 Air Well
- 2 " "
- 3 " "
- 4 Downie Deep Well Pump.
- 5 Cook Deep Well Pump.
- 6 " " " "
- 7 Air Compressor.
- 8 Gordon and Maxwell Pressure Pump.
- 9 Worthington Pressure Pump.
- 10 Boilers
- 11 Coal.
- 12 Air Receiver.
- 13 Reservoir.



○6



Champaign and Urbana Water Company

Plate 14.

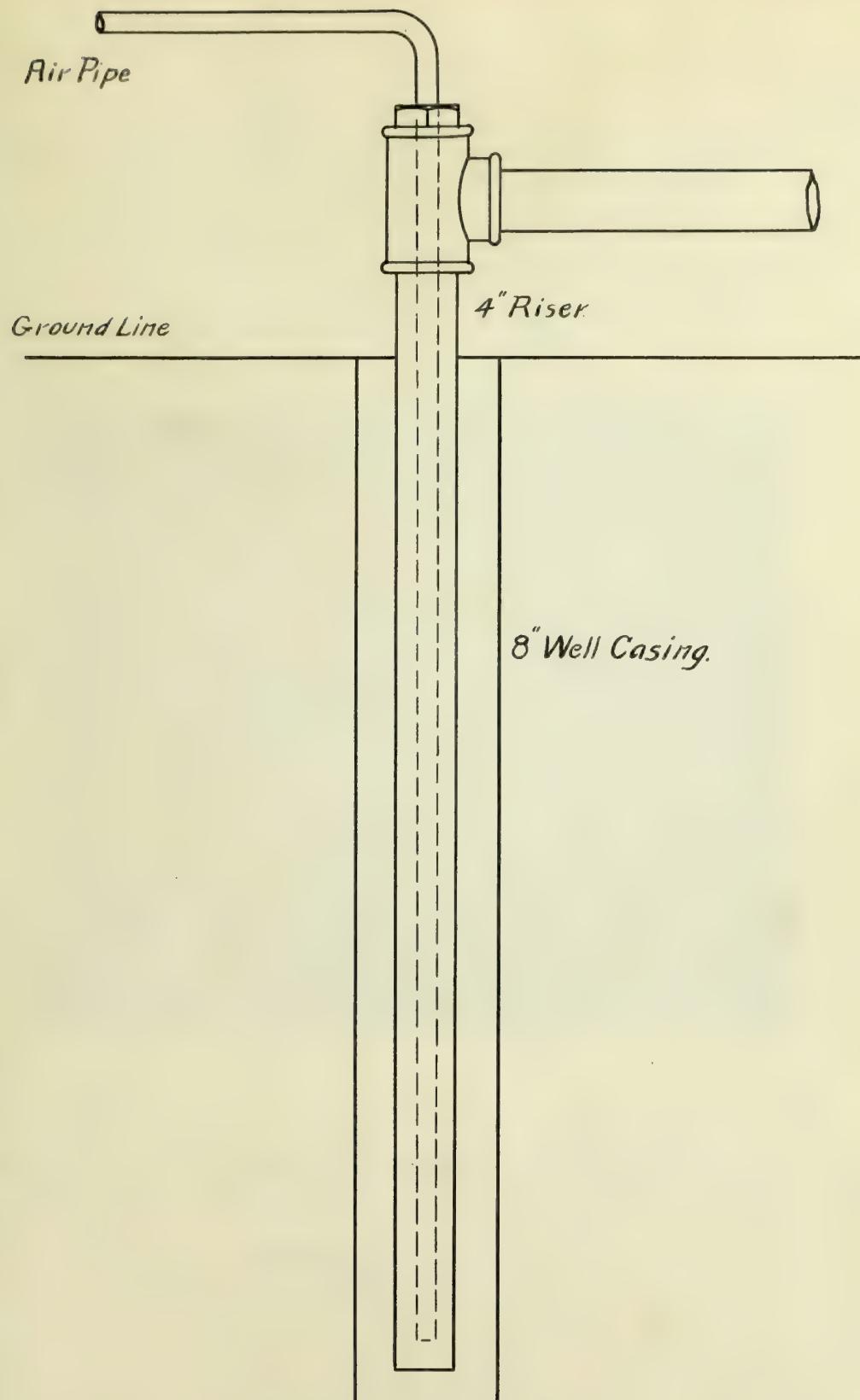
in diameter. All of the air pipe is had an 8 inch casting in which is casted a 4 inch vertical riser with an air pipe 1-1/2 inches in diameter inside of it. Well number 2, which gave the most trouble, was used to discharge into a "Measuring Tank" for a test. Table 11 gives a photograph showing the measuring tank, and pumping line to it from this well. An air pipe was placed in the measuring tank about 10 feet from well number 2.

Measurements were made at this point. Previous to the experiment some readings were taken in order to learn the general dimensions of the well. Table 11 gives the reading and dimensions of the well. Well number 2 is called "the Air Pumping Well".

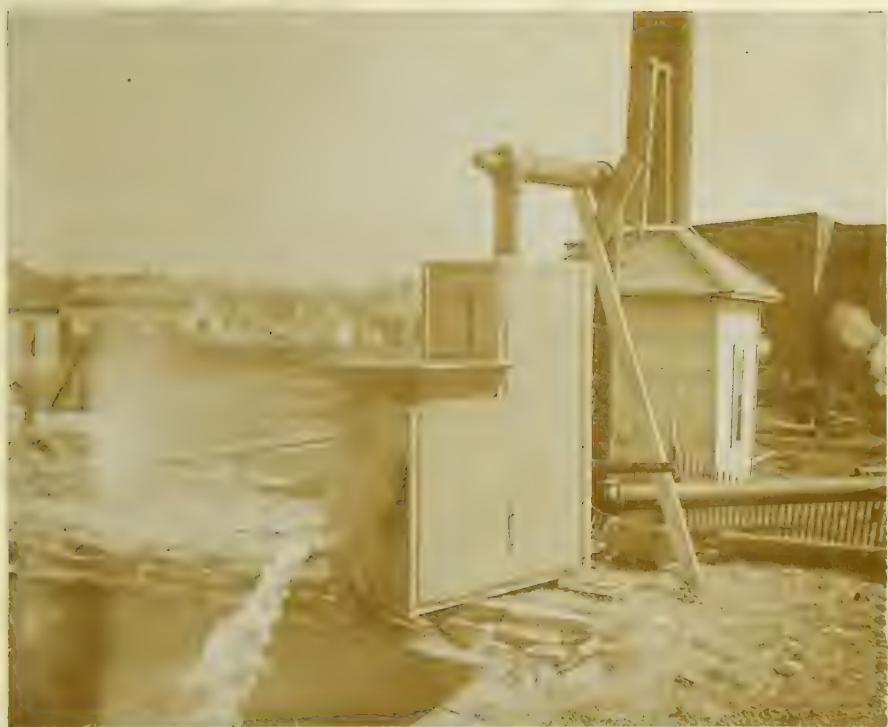
Table 11.

"Readings Taken at Air Pump Well in Order to Learn the Dimensions for Different Air Pressure and Speeds of the Compressor.

Dimensions of Air Pressure in inches. (Inches of Water)	Rate of Pumping in Gallons per minute.	Rate of Pumping in Gallons per minute.
74	.00	50.00
75	.50	12.00
76	.70	13.00
77	.70	10.00
78	.70	74.31
79	.70	74.31
80	.70	74.31
81	.70	74.31
82	.70	74.31
83	.70	74.31
84	.70	74.31
85	.70	74.31
86	.70	74.31
87	.70	74.31
88	.70	74.31
89	.70	74.31
90	.70	74.31
91	.70	74.31
92	.70	74.31
93	.70	74.31
94	.70	74.31
95	.70	74.31
96	.70	74.31
97	.70	74.31
98	.70	74.31
99	.70	74.31
100	.70	74.31
101	.70	74.31
102	.70	74.31
103	.70	74.31
104	.70	74.31
105	.70	74.31
106	.70	74.31
107	.70	74.31
108	.70	74.31
109	.70	74.31
110	.70	74.31
111	.70	74.31
112	.70	74.31
113	.70	74.31
114	.70	74.31
115	.70	74.31
116	.70	74.31
117	.70	74.31
118	.70	74.31
119	.70	74.31
120	.70	74.31
121	.70	74.31
122	.70	74.31
123	.70	74.31
124	.70	74.31
125	.70	74.31
126	.70	74.31
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130	.70	74.31
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135	.70	74.31
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137	.70	74.31
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455	.70	74.31
456	.70	74.31
457	.70	74.31
458	.70	74.31
459	.70	74.31
460	.70	74.31
461	.70	74.31
462	.70	74.31
463	.70	74.31
464	.70	74.31
465	.7	



Air Well Piping at the Urbana Water Works.



Measuring Tank for Jet Meter, at Pumping Station.

Urbana, Illinois.

Plate 16.

A test was made with the air supply shut off from the compressor to the air receiver, and with the pump and pump inlet valve in use. In this test the amount of water at different air pressures and different air volumes was found. Observations were taken from both the pump and the air receiver compressor. In the second test all of the data were recorded and cards taken from the compressor so that the work done in it was very under normal conditions, and the second test was made March 31st, 1900. Additional measurements were taken to the well used in order to read the measurements. This made the distance from the well to be measured 20 feet and the depth of submersion about 50 feet. These measurements were made when the well was not in operation. It was intended to measure the depth to the water level in the well, directly, by means of a float. This was attempted but did not succeed, given on the reason, that the float was suspended at a distance from the well opening, and by rounding the distance, water level the float used was caught between the pipes and one from the string to which it was fastened. The test was in running the compressor at different speeds and noting the pressure at the well, the amount of discharge and at the same time taking indicator cards from the compressor. From this were found the cubic feet of free air per minute, and the gallons of water per minute. Table 12 gives the results of this test.

It was intended to find the efficiency of the lift for different volumes of air used and different discharges of water.

the water in this case in the height of water raised times the area it is raised, divided by the total area of the air discharge of the compressor. As the water level in the well could not be taken for the different discharges this could not be done.

Table 12.

Water Discharged by Air Well Number 2 with different Air Pressures

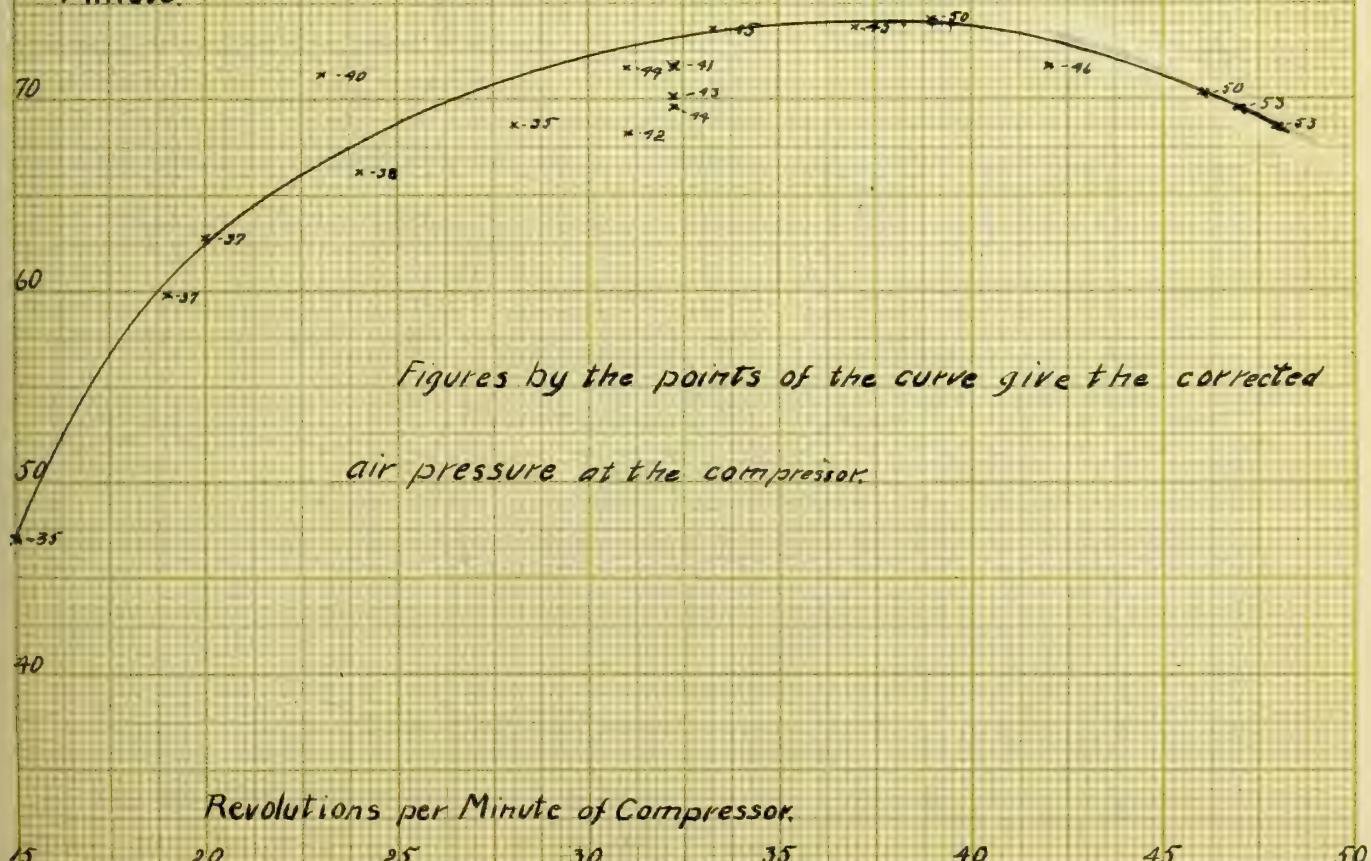
Barometric pressure 29.92 in. of mercury
Air Gauge (Air) Pressure. Pressure of air after raised.
Feeling at Gauge reading per min.
Compressor. Readings in feet, cubic feet (Gallons per
Pounds. Air pressure feet.
* Well (Frogs) feet. Air pressure feet.
Four cubic feet.

Barometric Pressure	Air Gauge Pressure	Feeling at Gauge	Compressor	Well (Frogs)
29.92	29.92	29.92	29.92	29.92
29.80	29.80	29.80	29.80	29.80
29.68	29.68	29.68	29.68	29.68
29.56	29.56	29.56	29.56	29.56
29.44	29.44	29.44	29.44	29.44
29.32	29.32	29.32	29.32	29.32
29.20	29.20	29.20	29.20	29.20
29.08	29.08	29.08	29.08	29.08
28.96	28.96	28.96	28.96	28.96
28.84	28.84	28.84	28.84	28.84
28.72	28.72	28.72	28.72	28.72
28.60	28.60	28.60	28.60	28.60
28.48	28.48	28.48	28.48	28.48
28.36	28.36	28.36	28.36	28.36
28.24	28.24	28.24	28.24	28.24
28.12	28.12	28.12	28.12	28.12
28.00	28.00	28.00	28.00	28.00
27.88	27.88	27.88	27.88	27.88
27.76	27.76	27.76	27.76	27.76
27.64	27.64	27.64	27.64	27.64
27.52	27.52	27.52	27.52	27.52
27.40	27.40	27.40	27.40	27.40
27.28	27.28	27.28	27.28	27.28
27.16	27.16	27.16	27.16	27.16
27.04	27.04	27.04	27.04	27.04
26.92	26.92	26.92	26.92	26.92
26.80	26.80	26.80	26.80	26.80
26.68	26.68	26.68	26.68	26.68
26.56	26.56	26.56	26.56	26.56
26.44	26.44	26.44	26.44	26.44
26.32	26.32	26.32	26.32	26.32
26.20	26.20	26.20	26.20	26.20
26.08	26.08	26.08	26.08	26.08
25.96	25.96	25.96	25.96	25.96
25.84	25.84	25.84	25.84	25.84
25.72	25.72	25.72	25.72	25.72
25.60	25.60	25.60	25.60	25.60
25.48	25.48	25.48	25.48	25.48
25.36	25.36	25.36	25.36	25.36
25.24	25.24	25.24	25.24	25.24
25.12	25.12	25.12	25.12	25.12
25.00	25.00	25.00	25.00	25.00
24.88	24.88	24.88	24.88	24.88
24.76	24.76	24.76	24.76	24.76
24.64	24.64	24.64	24.64	24.64
24.52	24.52	24.52	24.52	24.52
24.40	24.40	24.40	24.40	24.40
24.28	24.28	24.28	24.28	24.28
24.16	24.16	24.16	24.16	24.16
24.04	24.04	24.04	24.04	24.04
23.92	23.92	23.92	23.92	23.92
23.80	23.80	23.80	23.80	23.80
23.68	23.68	23.68	23.68	23.68
23.56	23.56	23.56	23.56	23.56
23.44	23.44	23.44	23.44	23.44
23.32	23.32	23.32	23.32	23.32
23.20	23.20	23.20	23.20	23.20
23.08	23.08	23.08	23.08	23.08
22.96	22.96	22.96	22.96	22.96
22.84	22.84	22.84	22.84	22.84
22.72	22.72	22.72	22.72	22.72
22.60	22.60	22.60	22.60	22.60
22.48	22.48	22.48	22.48	22.48
22.36	22.36	22.36	22.36	22.36
22.24	22.24	22.24	22.24	22.24
22.12	22.12	22.12	22.12	22.12
22.00	22.00	22.00	22.00	22.00
21.88	21.88	21.88	21.88	21.88
21.76	21.76	21.76	21.76	21.76
21.64	21.64	21.64	21.64	21.64
21.52	21.52	21.52	21.52	21.52
21.40	21.40	21.40	21.40	21.40
21.28	21.28	21.28	21.28	21.28
21.16	21.16	21.16	21.16	21.16
21.04	21.04	21.04	21.04	21.04
20.92	20.92	20.92	20.92	20.92
20.80	20.80	20.80	20.80	20.80
20.68	20.68	20.68	20.68	20.68
20.56	20.56	20.56	20.56	20.56
20.44	20.44	20.44	20.44	20.44
20.32	20.32	20.32	20.32	20.32
20.20	20.20	20.20	20.20	20.20
20.08	20.08	20.08	20.08	20.08
20.96	20.96	20.96	20.96	20.96
20.84	20.84	20.84	20.84	20.84
20.72	20.72	20.72	20.72	20.72
20.60	20.60	20.60	20.60	20.60
20.48	20.48	20.48	20.48	20.48
20.36	20.36	20.36	20.36	20.36
20.24	20.24	20.24	20.24	20.24
20.12	20.12	20.12	20.12	20.12
20.00	20.00	20.00	20.00	20.00
19.88	19.88	19.88	19.88	19.88
19.76	19.76	19.76	19.76	19.76
19.64	19.64	19.64	19.64	19.64
19.52	19.52	19.52	19.52	19.52
19.40	19.40	19.40	19.40	19.40
19.28	19.28	19.28	19.28	19.28
19.16	19.16	19.16	19.16	19.16
19.04	19.04	19.04	19.04	19.04
18.92	18.92	18.92	18.92	18.92
18.80	18.80	18.80	18.80	18.80
18.68	18.68	18.68	18.68	18.68
18.56	18.56	18.56	18.56	18.56
18.44	18.44	18.44	18.44	18.44
18.32	18.32	18.32	18.32	18.32
18.20	18.20	18.20	18.20	18.20
18.08	18.08	18.08	18.08	18.08
17.96	17.96	17.96	17.96	17.96
17.84	17.84	17.84	17.84	17.84
17.72	17.72	17.72	17.72	17.72
17.60	17.60	17.60	17.60	17.60
17.48	17.48	17.48	17.48	17.48
17.36	17.36	17.36	17.36	17.36
17.24	17.24	17.24	17.24	17.24
17.12	17.12	17.12	17.12	17.12
17.00	17.00	17.00	17.00	17.00
16.88	16.88	16.88	16.88	16.88
16.76	16.76	16.76	16.76	16.76
16.64	16.64	16.64	16.64	16.64
16.52	16.52	16.52	16.52	16.52
16.40	16.40	16.40	16.40	16.40
16.28	16.28	16.28	16.28	16.28
16.16	16.16	16.16	16.16	16.16
16.04	16.04	16.04	16.04	16.04
15.92	15.92	15.92	15.92	15.92
15.80	15.80	15.80	15.80	15.80
15.68	15.68	15.68	15.68	15.68
15.56	15.56	15.56	15.56	15.56
15.44	15.44	15.44	15.44	15.44
15.32	15.32	15.32	15.32	15.32
15.20	15.20	15.20	15.20	15.20
15.08	15.08	15.08	15.08	15.08
14.96	14.96	14.96	14.96	14.96
14.84	14.84	14.84	14.84	14.84
14.72	14.72	14.72	14.72	14.72
14.60	14.60	14.60	14.60	14.60
14.48	14.48	14.48	14.48	14.48
14.36	14.36	14.36	14.36	14.36
14.24	14.24	14.24	14.24	14.24
14.12	14.12	14.12	14.12	14.12
14.00	14.00	14.00	14.00	14.00
13.88	13.88	13.88	13.88	13.88
13.76	13.76	13.76	13.76	13.76
13.64	13.64	13.64	13.64	13.64
13.52	13.52	13.52	13.52	13.52
13.40	13.40	13.40	13.40	13.40
13.28	13.28	13.28	13.28	13.28
13.16	13.16	13.16	13.16	13.16
13.04	13.04	13.04	13.04	13.04
12.92	12.92	12.92	12.92	12.92
12.80	12.80	12.80	12.80	12.80
12.68	12.68	12.68	12.68	12.68
12.56	12.56	12.56	12.56	12.56
12.44	12.44	12.44	12.44	12.44
12.32	12.32	12.32	12.32	12.32
12.20	12.20	12.20	12.20	12.20
12.08	12.08	12.08	12.08	12.08
11.96	11.96	11.96	11.96	11.96
11.84	11.84	11.84	11.84	11.84
11.72	11.72	11.72	11.72	11.72
11.60	11.60	11.60	11.60	11.60
11.48	11.48	11.48	11.48	11.48
11.36	11.36	11.36	11.36	11.36
11.24	11.24	11.24	11.24	11.24
11.12	11.12	11.12	11.12	11.12
11.00	11.00	11.00	11.00	11.00
10.88	10.88	10.88	10.88	10.88
10.76	10.76	10.76	10.76	10.76
10.64	10.64	10.64	10.64	10.64
10.52	10.52	10.52	10.52	10.52
10.40	10.40	10.40	10.40	10.40
10.28	10.28	10.28	10.28	10.28
10.16	10.16	10.16	10.16	10.16
10.04	10.04	10.04	10.04	10.04
9.92	9.92	9.92	9.92	9.92
9.80	9.80	9.80	9.80	9.80
9.68	9.68	9.68	9.68	9.68
9.56	9.56	9.56	9.56	9.56
9.44	9.44	9.44	9.44	9.44
9.32	9.32	9.32	9.32	9.32
9.20	9.20	9.20	9.20	9.20
9.08	9.08	9.08	9.08	9.08
8.96	8.96	8.96	8.96	8.96
8.84	8.84	8.84	8.84	8.84
8.72	8.72	8.72	8.72	8.72
8.60	8.60	8.60	8.60	8.60
8.48	8.48	8.48	8.48	8.48
8.36	8.36	8.36	8.36	8.36
8.24	8.24	8.24	8.24	8.24
8.12	8.12	8.12	8.12	8.12
8.00	8.00	8.00	8.00	8.00
7.88	7.88	7.88	7.88	7.88
7.76	7.76	7.76	7.76	7.76
7.64	7.64	7.64	7.64	7.64
7.52	7.52	7.52	7.52	7.52
7.40	7.40	7.40	7.40	7.40
7.28	7.28	7.28	7.28	7.28
7.16	7.16	7.16	7.16	7.16
7.04	7.04	7.04	7.04	7.04
6.92	6.92	6.92	6.92	6.92
6.80	6.80	6.80	6.80	6.80
6.68	6.68	6.68	6.68	6.68
6.56	6.56	6.56	6.56	6.56
6.44	6.44	6.44	6.44	6.44
6.32	6.32	6.32	6.32	6.32
6.20	6.20	6.20	6.20	6.20
6.08	6.08	6.08	6.08	6.08
5.96	5.96	5.96	5.96	5.96
5.84	5.84	5.84	5.84	5.84
5.72	5.72	5.72	5.72	5.72
5.60	5.60	5.60	5.60	5.60
5.48	5.48	5.48	5.48	5.48
5.36	5.36	5.36	5.36	5.36
5.24	5.24	5.24	5.24	5.24</

Plot of Values Given in Table 12.

80. Water Raised.

Gallons per
Minute.



about 10,000 feet above sea level, and had been in use for a time in the air system of an engine. It was originally a twin valve but had been replaced by a vacuum double valve. The engine developed about 100 horse-power at 600 gallons per twenty four hours. As far as the experiments of the case the efficiency to be found for the ratios of discharge according to the water level may be inferred. These results are given in Table 17.

Table 17

Ratio of Work of Water at Various Water Levels to the Distance

Water Level, in the Head, to Develop the Unit.

Water Level, in the Head, to Develop the Unit.	Work of Water at Various Water Levels	Efficiency %.
100 ft.	100 ft.	100
110 ft.	110 ft.	91
120 ft.	120 ft.	83
130 ft.	130 ft.	77
140 ft.	140 ft.	72
150 ft.	150 ft.	68
160 ft.	160 ft.	65
170 ft.	170 ft.	62
180 ft.	180 ft.	60
190 ft.	190 ft.	58
200 ft.	200 ft.	56
210 ft.	210 ft.	54
220 ft.	220 ft.	52
230 ft.	230 ft.	50
240 ft.	240 ft.	48
250 ft.	250 ft.	46
260 ft.	260 ft.	44
270 ft.	270 ft.	42
280 ft.	280 ft.	40
290 ft.	290 ft.	38
300 ft.	300 ft.	36
310 ft.	310 ft.	34
320 ft.	320 ft.	32
330 ft.	330 ft.	30
340 ft.	340 ft.	28
350 ft.	350 ft.	26
360 ft.	360 ft.	24
370 ft.	370 ft.	22
380 ft.	380 ft.	20
390 ft.	390 ft.	18
400 ft.	400 ft.	16
410 ft.	410 ft.	14
420 ft.	420 ft.	12
430 ft.	430 ft.	10
440 ft.	440 ft.	8
450 ft.	450 ft.	6
460 ft.	460 ft.	4
470 ft.	470 ft.	2
480 ft.	480 ft.	1
490 ft.	490 ft.	0.5
500 ft.	500 ft.	0.2

the greatest elevation of the water level that might be expected the ratio in no case could be hardly increased to far one third of the amount given. This shows that the ratio of the work of the rising water, to that done in the air cylinder, can hardly exceed a value of one third per cent. This agrees in general with the results in some of the experiments made by Professor Broen in America. That is, as the ratio of the water lift to that of the

conditions mentioned, because of the low pressure, the diffuser efficiency is low. Again, the amount of free air is in proportion of the air velocity losses. This also is due partly to the increased air velocity mentioned above. Then the compressor is altogether too ~~large~~ ^{small} for one well, that is, gives too great a discharge of air, and the efficiency was probably decreased a great deal by this reason.

Test Number 2, April 2nd, 1902.

Second test was an efficiency test of the compressor working under normal conditions, namely, full bore of the wells. The general dimensions of the compressor and the results of the test are given below.

Builder's Name: Stillwell - Pierce & Britton
Wadsworth, Ohio.

Size of steam cylinder, high pressure

" " " " 160

" " " " 160

Dimensions of cylinder

" " " " 160

" " " " 160

" expansion valve and ---

Weight of compressor

3600 pounds.

Compressor is built with a single cylinder and the air is compressed in two stages. The first stage is compressed by an expansion valve in used on the high pressure cylinder and an expansion valve on the low pressure cylinder.



Air Compressor
at Pumping Station Urbana, Ill.

Plate 17.

given the total effective pressure across the two air cylinders. The total effective pressure is calculated as follows, by multiplying the area of each cylinder by its length and multiplying by the cosine of the angle.

21.50 on the high pressure steam cylinder

steam cylinder, and 40 on the low pressure steam cylinder

.75 and .9 give a set of t

air cylinders. There is quite a large drop in

pressure between the high and low pressure steam cylinders,

indication between the high and low pressure cylinders

that the high pressure cylinder does twice as much work as the low pressure cylinder.

Table 6 gives the Indicated Horse Power (I.H.P.) of the air cylinders and also the ratios between the total air and maximum powers. This last result is the mechanical efficiency of the cylinders.

Actual Quantities.

1. Condition of test

2. Actual revolutions of compressor -----

3. Weight of free air displaced ----- pounds

4. Indicated consumption, (Sand water to No. 1 air) ----- pounds

5. Water used in jackets of air cylinders ----- pounds

Estimated Quantities.

1. Indicated horse power of air cylinders -----

2. Indicated horse power of steam cylinders -----

3. Actual consumption of air (in lbs.) -----

4. Actual consumption of steam (in lbs.) -----

5. Weight of water used in jackets of air cylinders -----

TABLE 14.
Mean Effective Pressures.

Number.	R. P. M.	Air Press- ure at Com- press- or Pounds.	Steam Press- ure. Pounds.	Steam Cylinders.				Air Cylinders.			
				High Pressure.		Low Pressure.		North		South.	
				Head.	Crank.	Head.	Crank.	Head.	Crank.	Head.	Crank.
1	31	40	70	47.95	47.00	8.52	7.28			20.36	19.88
2	32	45	70	47.95	46.85	9.79	9.04	22.64	21.72	21.28	18.96
3	64	50	85	50.00	48.00	11.04	10.78	25.60	24.76	25.20	21.04
4	65	50	85	50.50	48.80	10.92	10.87	25.40	24.16	24.52	20.76
5	66	48	82	49.70	47.35	10.40	10.40	25.44	24.16	24.80	23.20
6	66	50	84	50.50	46.90	10.60	10.00	25.48	24.20	26.00	23.44
7	62	50	83	51.90	49.65	10.40	9.80	24.96	23.60	24.12	20.28
8	46	45	77	50.00	48.45	9.20	8.80	24.96	23.40	23.96	20.84
9	51	45	78	50.00	48.30	9.60	9.00	25.00	23.40	24.12	21.08
10	58	48	83	50.50	48.45	10.56	10.15	24.64	24.56	24.64	24.00
11	52	45	80	50.00	48.25	10.32	9.60	25.36	24.16	23.96	21.76
12	57	48	83	50.00	48.95	10.78	9.72	26.08	24.52	25.12	23.16
13	56	48	82	49.50	49.50	9.84	9.60	25.36	24.16	24.60	21.76
14	57	48	82	49.65	47.50	10.80	9.51	25.52	24.08	24.88	23.16
15	50	45	80	49.45	48.00	10.30	9.60	24.00	22.40	24.68	21.88
16	53	46	81	48.75	48.50	10.80	9.60	25.60	22.56	24.64	21.88
17	52	45	80	49.44	47.50	11.06	10.00	25.20	24.40	24.92	21.88

Form D-2 10-98-5 M-W.

SCALE **50**.....SIZE CYL **12" X 18"**.....

M. E. LABORATORY U. OF I.

ENGINE.....

TIME OR NO. **7**.....

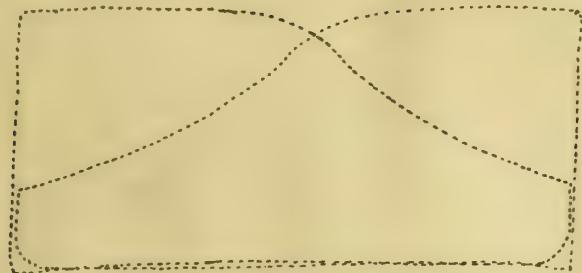
BOILER PRES.

DATE

END.....

R. P. M.

VAC. GAUGE



NOTE: TAKE DIAGRAM ON THIS SIDE OF PAPER

*Head**High Pressure.**Crank.*

Form D-2 4-97-5 M-W.

SCALE **20**.....SIZE CYL **18" X 18"**.....

M. E. LABORATORY U. OF I.

ENGINE.....

TIME OR NO. **7**.....

BOILER PRES.

DATE

END.....

R. P. M.

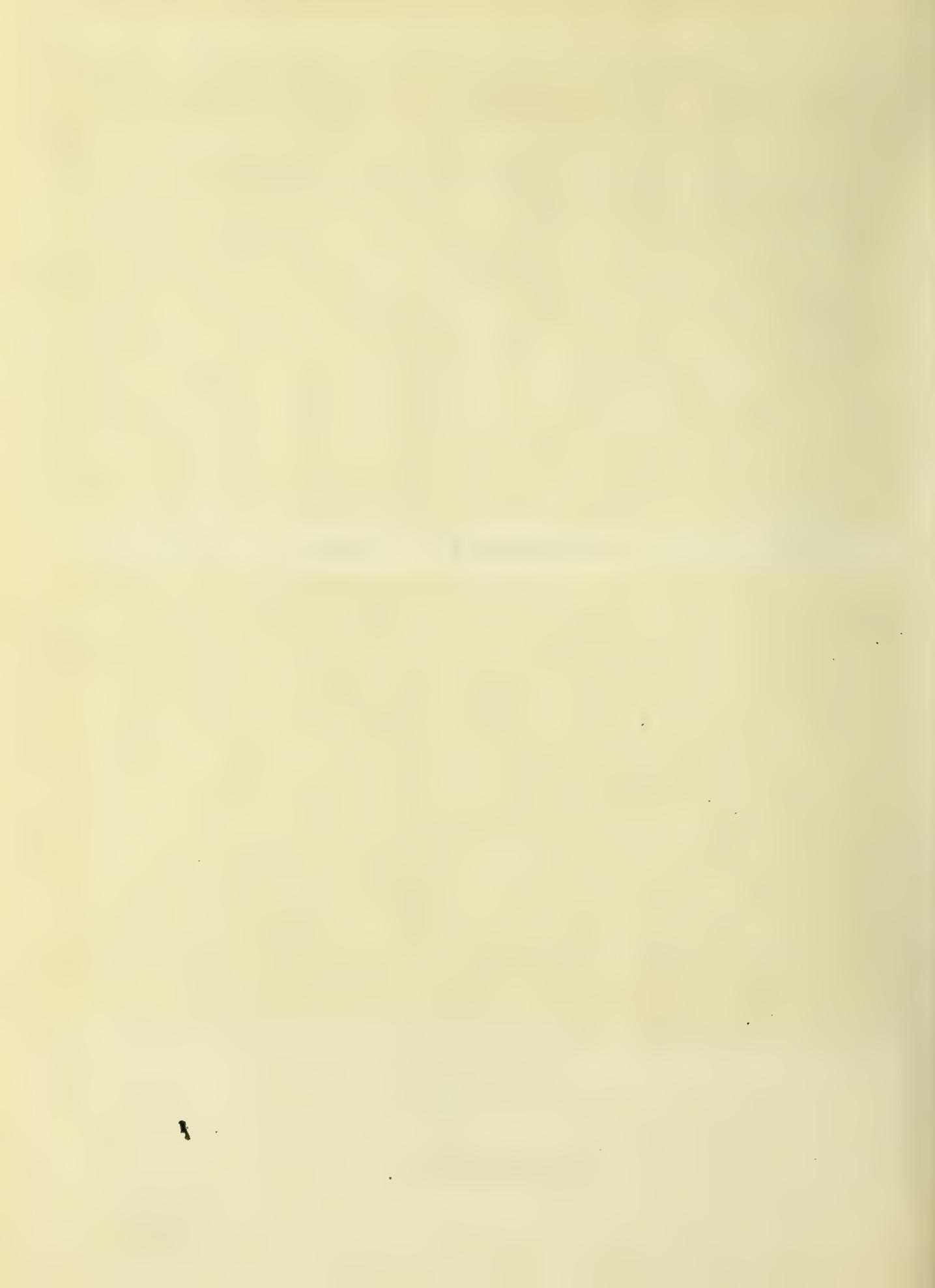
VAC. GAUGE



NOTE: TAKE DIAGRAM ON THIS SIDE OF PAPER.

*Low Pressure.**Steam Cards.*

Plate 18.



Form D-2-10-98-5 M-W.

SCALE **40**.....

BOILER PRES.

END.....

R. P. M.

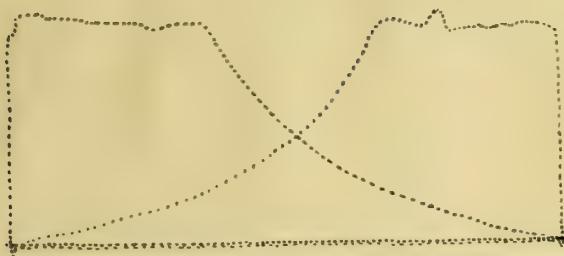
VAC. GAUGE.....

M. E. LABORATORY U. OF I.

SIZE CYL **19" x 18"**

ENGINE.....

DATE.....

TIME OR NO. **7**

NOTE: TAKE DIAGRAM ON THIS SIDE OF PAPER.

Head.

North Cylinder.

Crank.

Form D-2-4-97-5 M-W.

SCALE **40**.....

BOILER PRES.

END.....

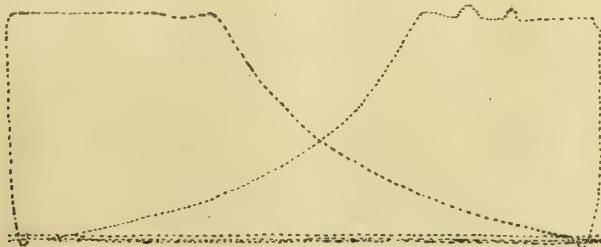
R. P. M.

VAC. GAUGE.....

M. E. LABORATORY U. OF I.

SIZE CYL **19" x 18"**

ENGINE.....

TIME OR NO. **7**

NOTE: TAKE DIAGRAM ON THIS SIDE OF PAPER.

South Cylinder.

Air Cards.

Plate 19.

TABLE 15.
Horse Powers.

Num- ber	Steam Cylinders.				Air Cylinders.				Total		Effi- ciency %
	High Pressure.		Low Pressure.		North		South.		Steam	Air	
	Head	Crank	Head	Crank	Head	Crank	Head	Crank			
1	7.43	7.28	3.01	2.58			4.41	4.31	20.30	17.44	85.90
2	7.42	7.26	3.45	3.19	4.86	4.60	4.67	4.02	21.32	18.15	85.12
3	16.25	15.60	8.18	7.99	11.57	10.95	11.39	9.32	49.02	43.23	90.02
4	16.41	15.86	8.09	8.04	11.57	10.99	11.15	9.44	48.40	43.15	89.10
5	16.40	15.62	7.85	7.85	11.67	10.87	11.37	10.54	47.72	44.45	91.68
6	16.67	15.51	8.00	7.55	11.93	10.54	11.69	9.89	47.73	44.05	90.02
7	15.57	14.90	7.30	6.93	10.76	9.98	10.36	8.57	44.79	39.67	84.05
8	11.50	11.14	4.82	4.62	7.91	7.50	6.58	6.52	32.08	28.61	89.21
9	12.75	12.32	5.78	5.24	8.85	8.14	8.53	7.33	36.09	32.85	91.02
10	14.64	14.05	6.87	6.02	9.72	9.52	9.89	9.50	41.58	38.63	93.14
11	13.00	12.55	6.12	5.51	9.18	8.58	8.66	7.72	37.18	34.14	91.82
12	14.25	13.95	7.00	6.32	10.34	9.48	9.99	8.96	41.52	38.77	93.30
13	13.86	13.86	6.29	6.12	9.86	9.18	9.54	8.26	40.13	36.84	91.82
14	14.15	13.84	7.02	6.48	10.01	9.30	9.50	8.96	41.19	37.77	91.64
15	12.36	12.00	5.92	5.97	8.33	7.62	8.38	7.44	35.75	31.77	88.87
16	12.90	12.85	6.52	5.80	9.42	8.16	9.06	7.93	37.87	34.57	91.52
17	12.85	12.35	6.56	5.93	9.10	8.68	8.99	7.77	37.69	34.54	91.64
Average									38.84	35.21	90.63

the air fluctuates away, so that the air pressure at the wells varies from time to time, on account of the loss through friction in the pipe line. The air passes through the pipe line at the rate of two cubic feet per second, number three. The friction loss is about one and one-half times the head loss. It has been estimated that under ordinary conditions number one and three will know not more than one and one-half times as much friction loss as number two, probably less often than a month. During the period of 24 hours number two raised 16,593.4 gallons of water or 2,074 gallons per hour. At the rate given above the three wells will raise 248,963.5 gallons per hour or 3,112 gallons per minute. This is 287.1 cubic feet of water raised from 11.1 per cent. on 100.3 per cent. of water or 100 per cent. of steam. This is no better than the results obtained from some "dead" dead well pump work, such as this taken from the "American Pumping Company" of New York:

From the results obtained it will be seen that the air lift at least is not the reliable article advocated by this company for pumping. This is due partly to the fact that the air lift is not a good pump, and also to the fact that the wells are not except in successful operation on the system. The chief reason for this is that the depth of the water in the wells is not great enough for the height the water has to be lifted.

1867 : 100 A New Method of Compressing Air.

1867 : 100 (5 p. 24. 1.) J. P. Prizell.

September 1877.

1877 : 100 Experiments on the Compression of Air by the

1877 : 105 Direct Action of Water.

September 1870. (100. 46. 26.) J. P. Prizell.

1878 : 100 The Air Lift Pump.

1878 : 100 (3p. 3d. 1t.)

1878 : 100 Historical. 1873 results of tests made by Prof. P. M. Rawball at Alameda, California.

1878 : 100 Pohle's Air Lift.

1878 : 100 (3p. 3d. 1t.)

1878 : 100 Notice of paper by R. E. Brown and Hans Behr.

1878 : 100

1878 : 100 Dr. Pohle's Air Lift Pump.

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1878 : 100 (6p. 3i. 2d. 4t.) H. C. Behr.

1878 : 100

1878 : 100

1878 : 100

1878 : 100 Pohle's Air Lift.

1878 : 100 (3p. 3d. 1t.)

1878 : 100

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The Theory of the Air Lift Pump.
(20p. 2d. 1f.) Prof. F. A. Harris.

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Pohle's Air Lift Pump.
(1-1/2p. 4f.) C. A. Statafeldt.

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The Air Lift Pump.
C. A. Statafeldt.

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The Air Lift.
(20. 2d. 3f.) Translation of paper by
Prof. F. Jossé in the
(1p. 5c) "Zeitschrift".

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The Air Lift Pump.
(20. 2d. 6d.) C. C. Lovvold.
Report of test at Rockford, Ill.

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The New Rockford Pumping Plant.
(1-1/2p. 2f. 3d.) Deep well pumps substituted for air lift.

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Raising Water by the Air Lift.

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Raising Water by the Air Lift.
(1p. 2f.) Plants at Rockford and Joliet, Ill.

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A Test of the Pohle Air Lift Pump
at De Kalb, Illinois.
(2/2p. 2d.) J. R. Merriam.

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Air Compressor, Dixon, Ill.,
Water Works.
(1/2p. 1f.)

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Improved air pump.

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Air Lift Pumping Station.

C. A. Improved Pneumatic Displacement Pumps.
4 : 598 (2-1/2p. 4i.)
March '99 Merrill Pneumatic Pump.

E. R. A Compressed Air Pumping Plant.
29 : 395 (1-1/2p. 2d.)
19 May '94. A mine at Plymouth, Pa. in which
ordinary steam pumps are run by
compressed air.

A. M. Pumping or Raising Water by
19 : 472 Compressed Air.
7 May '96. (1p.) Frank Richards.

E. & M.J. Compressed Air for Pumping.
59 : 314 (1p.) Frank Richards.
6 April '95. Protest against using compressed
air to run poor pumps.

C. A. Driving Pump by Compressed Air.
3 : 580 (6p. 6t.) William Cox.
Feb. '99. Gives formulae for finding amount of air
required to raise a given amount of water
when using direct acting pumps.





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